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BUBBLE REGIME TO MULTIBUBBLE REGIME

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SUMMARY

A photographic study was made of over 5000 bubbles in the nucleate boiling of methanol and water on a narrow heating strip at various heat fluxes and degrees of subcooling. The results showed that transition from the discrete-bubble regime to the multibubble regime was gradual. The fraction of heating area covered by multibubbles increases with increasing heat flux and is predictable. The area fraction is a Poisson function of the product of the mean area of influence of single bubbles and the instantaneous population density.

INTRODUCTION

Because nucleate boiling is recognized as a very effective means of heat transfer, a tremendous amount of effort has been directed toward the understanding of this interesting phenomenon. Among such efforts, a good part has been devoted to the study of bubbles. To facilitate observation, studies usually were made on discrete bubbles. Thus, the formulation of theories on nucleate boiling was on the basis of the information derived from discrete bubbles (refs. 1 to 3). These theories were generally applied to the entire regime of nucleate boiling. Recently, however, it has been becoming more and more clear that there actually exist several subdivisions in nuclear boiling, namely, a discrete bubble regime, a merging bubble regime, and perhaps a vapor-patch regime (refs. 4 to 7). It is evident that theories should be developed to deal with each region individually, as well as to predict the transition from one region to another.

It is the purpose of this report to study the transition of the discrete-bubble regime to the merging-bubble regime. In reference 8, an abrupt transition point was proposed, while in reality the transition is gradual and continuous. This report will show how the area covered by merging bubbles gradually increases with increasing heat flux and that the area fractions for merging bubbles can be related with other parameters such as bubble size and instantaneous bubble population. The hope is that, if the area fractions covered by the merging bubbles and the discrete bubbles at a given condition are known, the overall heat-transfer coefficient can be synthesized by weighing the contributions due to the two bubbling mechanisms according to their

respective area fractions.

The experimental phase of this work consisted of a photographic study of nucleate boiling of methanol and water on a 1/16- by 3/4-inch heating strip under 1 atmosphere pressure. The resulting data were then analyzed by assuming a Poisson distribution of bubbles.

SYMBOLS

A	area
a	empirical area parameter used in equation (1)
a,b	empirical parameters used for bubble growth rate $R = at^b$
D	bubble diameter
f	bubble generating frequency
\mathcal{F}	bubble fraction
g	gravitational acceleration
h	total number of all single bubbles studied in one roll of film
K	thermal conductivity
k	number of sample frames
L	length of heating strip
M	average number of sites per cell
N	site population
n	instantaneous bubble population
P	probability according to Poisson function
q	heat flux
R	bubble radius
\dot{R}	bubble growth rate, dR/dt
s	standard deviation associated with average area fraction of merging bubbles
ΔT_{sub}	subcooling temperature difference between saturation and bulk temperatures

ΔT_w	temperature difference between surface and bulk
t	time
t_g	bubble growth period
t_w	waiting period
W	half-width of heating strip
X	number of bubble sites per cell
x	number of bubbles in a cell
β	contact angle, radians
γ	surface tension
δ	thermal layer thickness
λ	latent heat of vaporization
μ	average number of bubbles per cell
ρ	density
σ	theoretical standard deviation
ϕ	area fraction

Subscripts:

av	average
B	bubble
b	bubble base
calc	calculated
d	departure
exp	experimental
F	Fritz equation of bubble departure, equation (9)
l	liquid
m	merging bubbles or multibubbles
s	single bubble

sub subcooling

t total

v vapor

Superscript:

- average

LITERATURE SURVEY

As mentioned in the INTRODUCTION, bubble interference has been reported previously. The earliest mention of it was probably that found in reference 9. More recent experimental findings have been reported since then. In general, the bubble interference can be classified as one of two types, vertical interference and lateral interference. The vertical interference occurs between consecutive bubbles emitted from the same nucleation site in rapid succession. This type of bubble interference is called chain-bubble interference in reference 9. It is also reported in references 6, 8, 10, and 11. This type of bubble coalescence was the model utilized in reference 8 to derive the criterion for the transition from the discrete-bubble regime to the merging-bubble regime. Deissler used a similar model for an analysis of burnout heat flux (ref. 12). The lateral type of bubble coalescence (or mushroom bubbles according to ref. 4) is the interference between the neighboring bubbles due to close proximity. As observed in references 3, 4, and 13, a growing bubble, while still attached to the heating surface, merges with a neighboring bubble. This merging can be caused either by contact of two growing bubbles or by the up draft of a departing bubble. The area of influence of each bubble is roughly 2 bubble radii away from the nucleation center (refs. 3 to 5). In either case, the lateral-merging bubbles can be pictured as mushrooms with two or more stems. These stems are the places where vaporization occurs. This type of coalescence has been included in the boiling models postulated in references 3 to 5. As will be shown in the section RESULTS AND DISCUSSION, mushroom bubbles are far more frequently observed than chain bubbles. Therefore, the mushroom bubbles will be the ones discussed in this report.

Since the lateral coalescence is due to the interference of neighbors, the distribution of bubbles should be known. In the work of reference 14, it was found from the distribution of the sites on a boiling surface that the site population was distributed according to Poisson's equation

$$P_M(X) = \frac{e^{-M} M^X}{X!} \quad (1)$$

where $M = \bar{N}a/A$ and $X = N_a/A$, but no attempt was made to predict the population distribution a priori; instead, the cell area a was used strictly as an empirical parameter to fit the data with Poisson curves.

APPARATUS AND PROCEDURE

The test was carried on inside a 6-inch-diameter by 4-inch-high cylindrical tank made of stainless steel and provided with viewing windows. The tank had provisions for a fill, a drain, a pressure gage, electrical connections, thermocouple leads, and auxiliary heaters. The heater was a thin, electrically conductive, transparent coating $1/16$ -inch wide, and 1-inch long deposited on a 1- by 1- by $1/8$ -inch heat-resisting glass plate. The plate was mounted horizontally on a small bench with a mirror situated beneath the plate and inclined 45° . Thus, the camera aiming from a front window saw simultaneously a front view and a bottom view (through the mirror) of the image of any bubble generated on the heating surface. The plate was clamped down with two copper clamps, which also served as electrical leads. The actual heating area was $1/16$ by $3/4$ inch, since the two end areas were covered by the copper clamps (fig. 1).

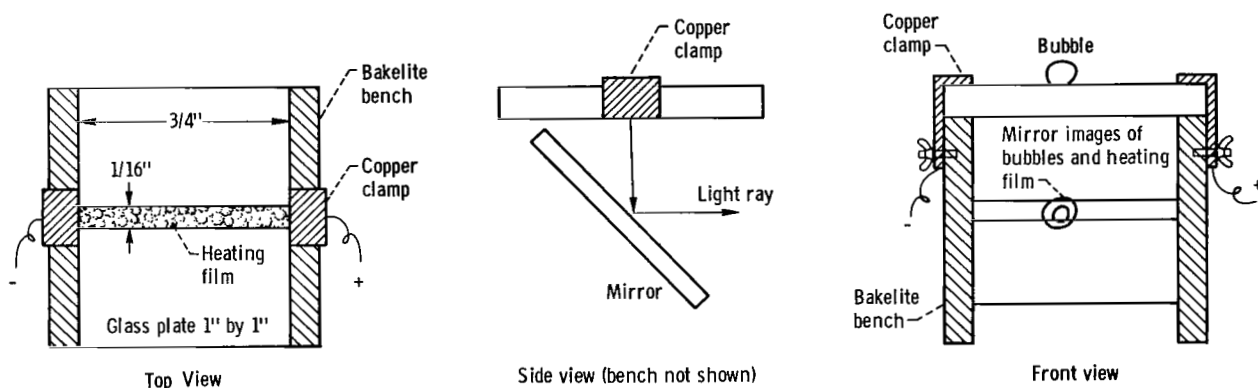


Figure 1. - Setup of heating element.

The $1/16$ -inch-wide strip was used instead of a wider heating area to ensure that no more than two rows of bubbles were generated. This arrangement was necessary to avoid confusion in the front view due to the presence of overlapping rows of bubbles. Originally, an alternating-current source was used, but because of the low heat capacity of the heating film, there were 120 cps temperature fluctuations on the heating surface. At lower heat flux, when bubble frequencies were low, this 120 cps fluctuation apparently did not have a serious effect. As the heat flux was increased and bubble frequency fell in the vicinity of 120 cps, however, the alternating-current fluctuation began to dictate the bubble frequency, and the bubbles began to grow in unison. Thus, only those runs where there was no apparent synchronization between bubbles and current waves were retained. Later, a direct-current source was used. Because of the high voltage applied to the electrodes (60 to 120 v), electrolysis would take place if water were used. Thus, only methanol was used for direct-current runs. At the beginning of a series of runs, the tank was loaded with a fresh batch of pure methanol or distilled water. The liquid was preheated to a desired temperature by the auxiliary heater. The bulk temperature was constantly monitored through thermocouple readings, and the temperature level was controlled by turning the auxiliary heaters on and off. The auxiliary heaters were always off while actual test runs were being carried out. The test heater would be turned on and set at a desired heat flux by varying the applied voltage, and then high-speed motion pictures (up to 5000 frames/sec) were taken.

The simultaneous viewing of bubble activities from front and bottom (mirror image) was deemed necessary to get the true picture of bubble interaction. Because of the difference in optical distance of the two views, however, it was extremely difficult to keep both views in sharp focus. Thus, the optical qualities of pictures were somewhat sacrificed. Because of such difficulties, studies were limited to those runs with a moderate amount of merging to maintain the accuracy of reading. The high-speed motion pictures were analyzed on a motion-picture analyzer. A total of 14 rolls were examined. For each roll, 50 to 100 frames were studied. The sample frames were selected by arbitrarily stopping the film 50 to 100 times at irregular intervals.

For each frame, information about each bubble present on the entire 3/4-by 1/16-inch heating surface was recorded. The raw data include

(1) The location and size of each bubble. The size or diameter of a bubble is defined as the width of a bubble at its widest part. In a few instances, a mushroom bubble could be a very wide hovering bubble overcasting a large area. In such cases, the bubble size is defined as the width of the bubble stem below the height of an average single bubble (see fig. 2).

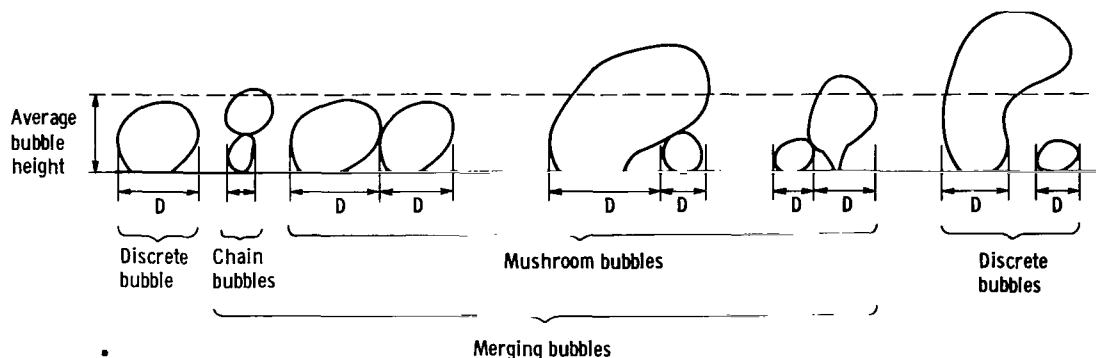


Figure 2. - Various configurations of bubbles.

(2) The classification of bubbles, namely, whether the bubble was a single bubble, or was merging with other bubbles. The criterion for the merging bubbles was the physical contact of two or more bubbles while at least one bubble was still attached to the heating surface.

(3) The number of active bubbles involved in a merging bubble.

(4) The total number of active bubbles n on that frame.

From the aforementioned raw data, calculations were made, and the following information was obtained:

(1) The average size of all the single bubbles recorded in the sample frames was determined. This average was expressed in terms of the area fraction of influence of single bubbles, averaged as a function of the total area or ϕ_s . The area of influence of the bubble ϕ_s was computed by the equations

$$\varphi_s = \frac{\pi D_s^2}{A_t} \quad \text{for } D_s < W \quad (2a)$$

and

$$\varphi_s = \frac{2 \left[W \sqrt{D_s^2 - W^2} + D_s^2 \sin^{-1} \frac{W}{D_s} \right]}{A_t} \quad \text{for } D_s > W \quad (2b)$$

- Area covered by bubble with radius R_s
- ▨ Area covered by influence of bubble (radius of twice the bubble radius; area fraction of bubble influence is φ_s)

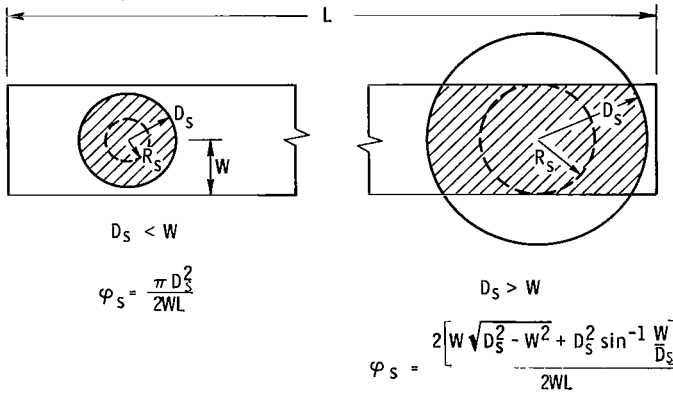


Figure 3. - Calculation of area fraction of heating strip covered by influence of bubble.

The shaded area in figure 3 are the areas of influence of single bubbles. Note that equation (2b) represents the area of a part of a circle with two segments cut off. The mean area fraction averaged over all the single bubbles is

$$\varphi_{s,av} = \frac{\sum_{i=1}^h \varphi_{s,i}}{h} \quad (2c)$$

where h is the total number of single bubbles studied in the roll.

(2) The average size of the area covered by a merging bubble in a frame was expressed as the area fraction φ_m , and was calculated by summing all the area fractions covered by each merging bubble in the same frame.

The area fraction of each merging bubble was also computed from equations (2a) and (2b), except that $D_m/2$ was used instead of D_s . The average area fraction of merging bubbles was computed over all the frames, or

$$\varphi_{m,av} = \frac{\sum_{i=1}^k \varphi_{m,i}}{k}$$

where k is the number of sample frames and $\varphi_{m,i}$ is the sum of all the area fractions of merging bubbles in the frame i . Also computed for each roll of film was the standard deviation s associated with the $\varphi_{m,av}$

$$s = \sqrt{\frac{\sum_{i=1}^k (\varphi_{m,av} - \varphi_{m,i})^2}{k}}$$

(3) The average instantaneous bubble population density n_{av} was taken for the total number of sample frames k .

The total number of active sites N seen in a given roll of film was also studied. The movie was projected on a paper and all the sites where bubbles had ever been generated were marked down. The range of conditions and the data are given in table I.

RESULTS AND DISCUSSION

General Description of Photographic Observation

Before the quantitative study of bubble interferences is discussed, the following qualitative descriptions should be given:

(1) The merging of bubbles was predominately due to lateral coalescence. The merging took place when one growing bubble got into the area of influence of a neighboring bubble. A detailed listing of bubble classification and raw data is contained in table II.

(2) The number of merging bubbles and the area covered by these merging bubbles increased with increases in both bubble size and instantaneous bubble population. With pressure and degrees of subcooling held constant, both the bubble size and the instantaneous bubble population increased with heat flux. Thus, increasing the heat flux means increasing the area of merging bubbles.

(3) The location of merging bubbles appeared to be random. For a given location, at one moment there could be no bubbles, one bubble, several discrete bubbles, or merging bubbles; however, the probability of having merging bubbles increased with increasing heat flux.

Analysis

Based on the general qualitative description of bubble interference observed photographically, a model will be postulated to account quantitatively for the area fraction covered by the merging bubbles. The analysis will be carried out in two steps: The first step will be to seek the relation between the area of a merging bubble and quantities such as the mean area of influence of a bubble and the instantaneous bubble population, provided the latter two are given. The second step will be to estimate the area of influence and the instantaneous bubble population from the more basic information such as heat flux, subcooling, and total bubble population (or site population). The pur-

pose is to estimate the area of merging bubbles from the aforementioned basic information.

Basic model. - The basic model for bubble interference is described in the following manner:

(1) Each bubble has an area of influence, which is the area within 1 bubble diameter of the nucleation center. This assumption is based on the observations made in reference 3.

(2) Since each bubble grows, the area of influence is based on the time-mean bubble size. This mean area of influence of a single bubble is considered as a cell. The heating surface is divided into such cells.

(3) Two bubbles will merge if one is located within the area of influence of the other.

(4) The bubbles are assumed to have a Poisson distribution.¹ This distribution is assumed to apply not only to site population as found in reference 14, but also to the instantaneous bubble population. Note that, at any moment, only part of the sites are actively occupied by bubbles, while the rest are in the waiting period.

Poisson distribution. - The following equation is used to express the previously postulated model in mathematical form:

$$P_{\mu}(x) = \frac{e^{-\mu} \mu^x}{x!} \quad (3)$$

where $P_{\mu}(x)$ is the percentage of cells each of which has x bubbles in it and the cell is defined as the mean area of influence of a single bubble. The average number of bubbles per cell is

$$\mu = \frac{n_{av}}{\frac{A_t}{A_s}} = \frac{n_{av}}{A_t} A_s = n_{av} \varphi_s \quad (4)$$

where A_s is the mean area of influence of a single bubble or the area of a cell, n_{av} is the average instantaneous bubble population on a total heating area A_t , and φ_s is the area fraction A_s/A_t . Note that equations (1) and (3) are similar in form except that the site population N is used in equation (1), while the instantaneous bubble population n is used in equa-

¹The assumption of Poisson distribution for the spatial distribution of bubbles makes possible the calculation of the area fraction for merging bubbles. If one is interested in the fraction of bubble population that is merging, however, an analysis of the clustering of bubbles can be found in appendix A.

tion (3) and that in equation (3) the cell area is defined as the area of influence of a bubble.

Since it is assumed that bubbles will merge when two or more bubbles are present in one cell, the percentage of cells that contain merging bubbles is

$$P_{\mu}(x > 2) = \sum_{x=2}^{\infty} P_{\mu}(x) \quad (5a)$$

or

$$P_{\mu}(x > 2) = 1 - P_{\mu}(0) - P_{\mu}(1) = 1 - e^{-n_{av}\phi_s}(1 + n_{av}\phi_s) \quad (5b)$$

Since $P_{\mu}(x > 2)$ is by definition the percentage of cells covered by two or more bubbles or merging bubbles, it is the area fraction covered by merging bubbles

$$\phi_m = P_{\mu}(x > 2) = 1 - e^{-n_{av}\phi_s}(1 + n_{av}\phi_s) \quad (6)$$

This equation will give the area fraction of merging bubbles if the mean instantaneous bubble population n_{av} and mean area of influence of a single bubble are known. These two terms can either be obtained experimentally or analytically. The next two sections constitute the second step of analysis, namely, determination of n_{av} and A_s analytically.

Mean area of influence of a single bubble. - According to the assumed basic model, the mean area of influence is the area within 1 bubble diameter of the nucleation center, and the bubble diameter is the time average of a growing bubble

$$D_{av} = \frac{1}{t_g} \int_0^{t_g} D(t) dt \quad (7a)$$

or

$$R_{av} = \frac{1}{t_g} \int_0^{t_g} R(t) dt \quad (7b)$$

The term bubble radius $R(t)$ can be obtained through bubble growth information. Although many theoretical equations are available, it is more convenient to use the empirical expression $R = at^b$, where $b = 0.4$ (ref. 15). Since the process of computing the time-average radius R_{av} involves integration of $R(t)$, small deviations in $R(t)$ usually will be evened out. Thus

$$R_{av} = \frac{a}{t_g} \int_0^{t_g} t^b dt = \frac{a t_g^b}{b+1} = \frac{R_d}{1+b} = \frac{R_d}{1.4} \quad \text{for } b = 0.4 \quad (7c)$$

As to the departure radius R_d , Staniszewski's empirical expression will be used

$$R_d = R_F(1 + 10.44 \dot{R}_d) \quad (8)$$

where \dot{R}_d is in feet per second, and R_d and R_F are in feet; R_F is the departure radius according to Fritz' equation

$$R_F = 0.4215 \beta \sqrt{\frac{2r}{g(\rho_l - \rho_v)}} \quad (9)$$

in which β is the contact angle in radians.

Unfortunately the growth rate at departure \dot{R}_d involved in equation (8) can no longer be calculated from the expression $R = at^b$, partly because the exponent b actually varies with time and partly because the coefficient a should be a function of an experimental condition such as heat flux, sub-cooling, pressure, or cavity size. Thus, an expression for the growth rate \dot{R} as a function of the test condition should be used.

Although many bubble growth equations are available, only a few consider the effect of the bulk turbulence by including terms that describe the thermal layer or the heat dissipation to the bulk. Among such equations are those proposed in references 3, 16, and 17. The equation in reference 16 would be quite convenient to use if both ΔT_w and q_w were known. Unfortunately, the growth expressions in references 3 and 17 are rather clumsy to use. If only the bubble growth rate at departure is of interest, however, the situation is somewhat simpler because of the fact that in the later stage of bubble growth the sensible heat stored in the superheated layer enveloping the bubble should have already been exhausted. Therefore, the bubble is losing heat to the surrounding bulk and receiving heat from the bubble base. (This heat may be in the form of evaporation of microlayer, as shown in ref. 18.) The bubble growth rate at departure can be easily derived, by following the procedure in reference 3, as

$$\dot{R} = \frac{1}{\lambda \rho_v} \left(\frac{A_b}{A_B} q - \frac{K \Delta T_{sub}}{\delta} \right) \quad (10)$$

where $A_b/A_B \approx 0.25$ if the bubble at departure can be assumed to be a truncated sphere with a contact angle between 45° to 60° (cf., ref. 3) and δ is the thermal-layer thickness. The information about thermal layer thickness of a boiling fluid is very meager, but there are a few measurements (refs. 6 and 19). Therefore, if the thermal layer thickness δ is known, by using

equations (8) to (10), the bubble departure size can be determined.

Instantaneous bubble population. - The instantaneous bubble population should be differentiated from the commonly used term "bubble population." The latter is actually a misnomer. When the bubble columns during the boiling or the number of aureoles left on a plate after boiling are counted, only the population of the bubble nucleation sites is determined, not the bubble population at any moment. The relation between site population N and the instantaneous bubble population n can be likened to that between the number of houses in a block and the number of families at home at a given moment. It is easy to see that these two populations can be related by the equation

$$n_{av} = \frac{t_{g,av}}{t_{g,av} + t_{w,av}} N = t_{g,av} f_{av} N \quad (11)$$

The variation of N as function of q has been reported in many places, and, unfortunately, the result varies widely. The difficulty stems from the diversity of surface condition and hysteresis (refs. 2, 6, and 20). Unless some characteristic parameter other than root-mean-square roughness of a surface can be found to account for cavity size distribution, it is futile to try to correlate N against q ; however, the site population N is still a quantity much easier to determine experimentally than the instantaneous bubble population n . Thus, it is still worthwhile to obtain n through N .

The mean frequency f_{av} can easily be determined through the expression in reference 16

$$fD = 0.59 \left[\frac{(\rho_l - \rho_v)gr}{\rho_l^2} \right]^{1/4} \quad (12)$$

which yields

$$f_{av} = \frac{0.59}{D_{d,av}} \left[\frac{(\rho_l - \rho_v)gr}{\rho_l} \right]^{1/4} \quad (13)$$

The time of growth period t_g can readily be calculated through

$$R_d = \int_0^{t_g} \dot{R} dt \quad (14)$$

provided $\dot{R}(t)$ and R_d are known. As mentioned before, an empirical expression can be used, namely,

$$R_d = at^b \quad (15)$$

$$\dot{R}_d = abt_g^{b-1} \quad (16)$$

$$\frac{R_d}{\dot{R}_d} = \frac{t_g}{b}$$

or

$$t_g = \frac{bR_d}{\dot{R}_d} \quad (17)$$

Thus from equations (8), (10), and (17) the growth period t_g can be calculated. Strictly speaking, equation (10) can be used to replace equation (16), only when the empirical form (eq. (16)) is identical to the analytical form (eq. (10)); however, an underestimated growth rate R tends to give an overestimated growth period t_g and an underestimated departure diameter D_d . The result is that the two errors tend to compensate each other in the product of mean bubble population and mean area of influence

$$n_{av}A_s = t_g \frac{(fD)_d}{D_d} \pi D_d^2 \quad (18)$$

Calculation of area fraction covered by influence of a single bubble
(calculation of $\phi_{s,av,calc}$ from $D_{av,calc}$). - The mean influence area fraction covered by a single bubble can be computed from the time-averaged diameter of a bubble D_{av} by using equations (2a) and (2b), except that D_{av} will be used in the place of D . The ϕ_s thus computed will be $\phi_{s,av,calc}$. Strictly speaking, $\phi_{s,av,calc}$ should be an average of $\phi_{s,calc}$ which, in turn, should be computed from $D(t)$ as shown in equation (2c). Since only an estimation was intended, $\phi_{s,av,calc}$ can be directly computed from $D_{av,calc}$.

Comparison of Experimental Data with Analysis

The quantitative result will be compared with the model derived in the section Analysis in two steps also. The first step will be to check whether the area fraction of merging bubbles ϕ_m based on the Poisson distribution (eq. (6)) can be used to relate ϕ_m with the experimental values of the mean area of influence of a single bubble $\phi_{s,exp}$ and the mean instantaneous bubble population $n_{av,exp}$. The second step will be to test whether equations (8) and (11) can be used to predict $\phi_{s,exp}$ and $n_{av,exp}$, respectively, and whether the calculated product $(\phi_s n_{av})_{calc}$ can be used to predict the merging bubble area fraction $\phi_{m,exp}$.

Relation between area fraction of merging bubbles ϕ_m against product of measured values of mean area of influence of single bubble and mean instantaneous bubble population $(n_{av}\phi_s)_{exp}$. - To test equation (6), $\phi_{m,av,exp}$ was

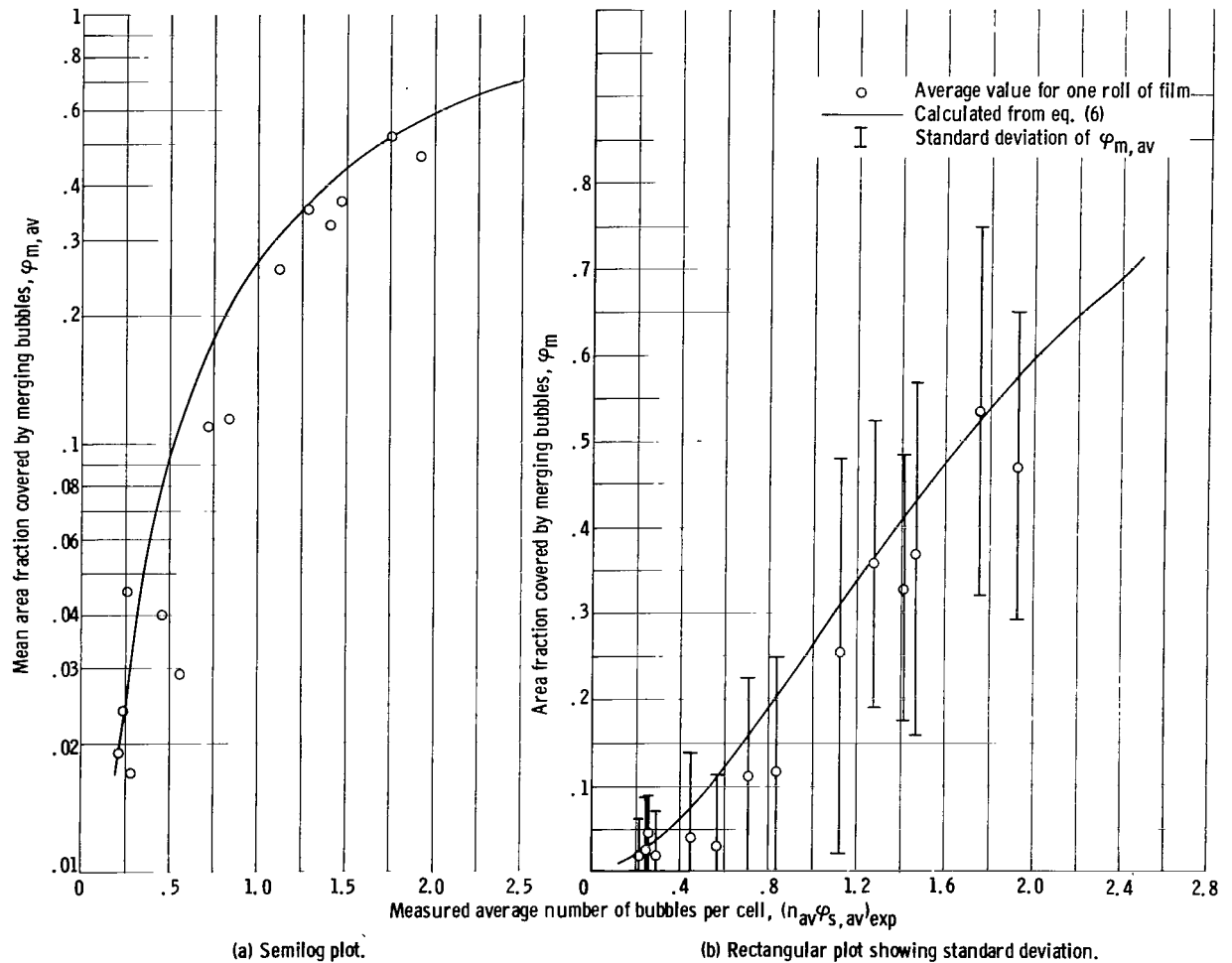


Figure 4. - Area fraction of merging bubbles as function of measured average number of bubbles per cell.

plotted against $(n_{av}\phi_{s,av})^{exp}$ (fig. 4(a)). The solid curve represents equation (6). Each circle represents the mean values obtained from one roll of film. Figure 4(b) shows a similar plot on rectangular coordinates to show the standard deviations associated with each average area fraction of merging bubbles for the samples studied. (The experimental values of standard deviation are compared with the theoretically expected values in appendix B.) Judging from the figures, the model is fairly close. Thus, if the mean bubble population n_{av} and the mean area of influence of single bubbles ϕ_s are given, the area covered by merging bubbles can be calculated. The values of n_{av} and $\phi_{s,av}$ can either be obtained experimentally in the same way that figure 4 was constructed, or they can be estimated from test conditions through bubble departure size, bubble growth rate, and frequency by using the available equations.

Comparison of calculated and measured bubble departure diameters $D_{d,cal}$ and $D_{d,exp}$. - To estimate $\phi_{s,av}$, it is necessary to know the departure diameter D_d . Equations (8) and (9) were used to compute D_d with departure growth

rate \dot{R}_d computed from equation (10). The thermal layer thickness δ used in equation (10) was determined from the experimental measurement of reference 10 by matching the heat-transfer coefficient for the case of water ($\delta \approx 10^{-3}$ ft). For the case of methanol, the thermal layer thickness was assumed to be 2×10^{-3} feet. The calculated values of D_d are then compared with the experimental ones derived through equation (7a). The comparison is shown in figure 5. It can be seen that most points are within a ± 20 percent error limit, which is about the same as the 25 percent error limit of equation (8).

Comparison of calculated and measured mean instantaneous bubble population $n_{av,calc}$ and $n_{av,exp}$. - To test equation (11), the mean instantaneous bubble population n_{av} was calculated from the experimentally determined site population N together with the calculated frequency f_{av} and growth period $t_{g,av}$. The bubble frequency f_{av} was calculated from equation (13) by using the calculated departure diameter $D_{d,calc}$. The growth period $t_{g,av}$ was calculated from equation (17) by using $D_{d,calc}$ and $R_{d,calc}$ (from eq. (10)). The comparison with $n_{av,exp}$ is shown in figure 6. The ± 60 percent error limits are also shown in the figure, which are the error limits associated with equation (12).

Comparison of measured merging bubble area fraction $\phi_{m,exp}$ with that obtained from the calculated average instantaneous bubbles per cell $(n_{av}\phi_s)_{calc}$. - By using equations (2a) and (2b), $\phi_{s,av}$ was computed from $D_{av,calc}$. In figure 7, the product $(\phi_{s,av}n_{av})_{calc}$ was plotted with the

average area fraction of merging bubbles $\phi_{m,av}$. Also shown in figure 7 is the theoretical curve from equation (6). Although there is scattering, the result is still

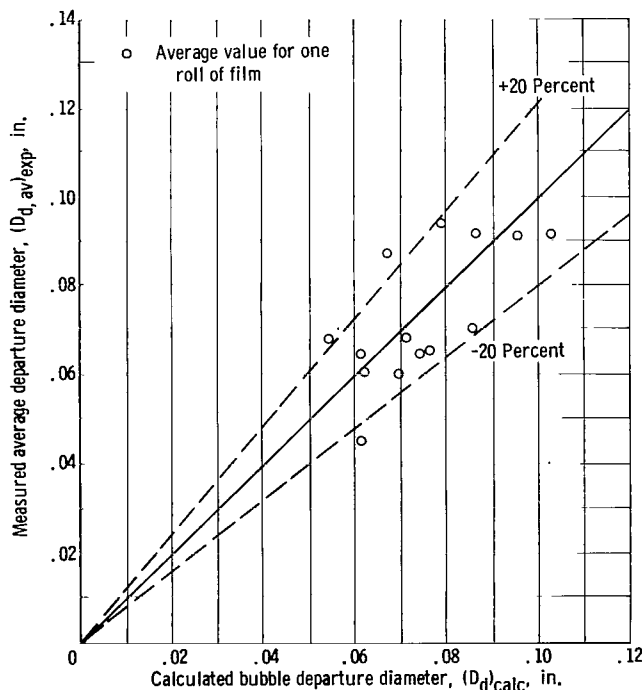


Figure 5. - Comparison of calculated and measured bubble departure diameters.

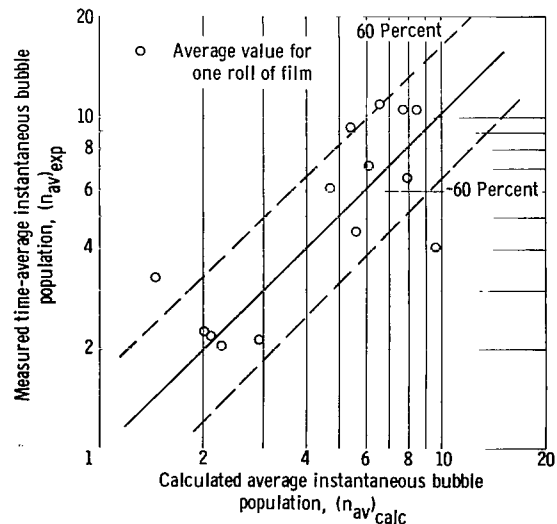


Figure 6. - Comparison of calculated and experimental values of average instantaneous bubble population.

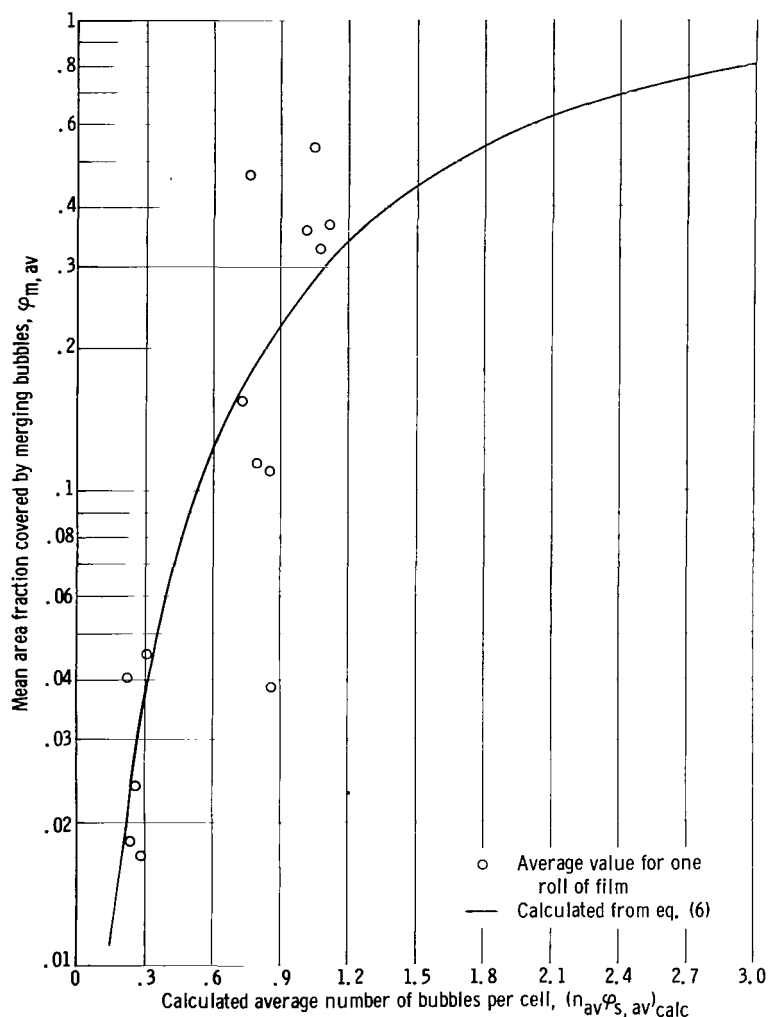


Figure 7. - Area fraction of merging bubbles as a function of calculated average number of bubbles per cell.

fractions of merging bubbles and discrete bubbles. Based on the result obtained from the boiling of methanol and water on a narrow heating strip, it is found that the transition from the discrete-bubble regime to the merging-bubble regime is gradual. Furthermore, the results showed that the area fraction of merging bubbles can be predicted satisfactorily from the Poisson distribution if the average number of bubbles per cell is known. (The cell is defined as the average area of influence of a single bubble.)

It is desirable to be able to determine the average number of bubbles per cell a priori. A method of estimating this item based on crude assumptions and empirical equations was proposed in this report. The maximum error associated with the estimated values was roughly 100 percent; this percentage might be due to the large errors introduced into the basic empirical equations. If a better method is available for estimating the bubble size and bubble popula-

quite gratifying considering all the crude assumptions being made and the large error limits associated with the empiricism of equations (8) and (12). Thus, it is shown that an estimate of the area covered by merging bubbles can be based on the test conditions (heat flux, pressure, subcooling, etc.) provided that the site population is known.

CONCLUDING REMARKS

In the nucleate-boiling regime, if both discrete bubbles and merging bubbles are present, the overall heat-transfer coefficient will have to be determined by considering the contribution due to both bubbling mechanisms. Even if the heat-transfer process of each mechanism were known, a weighting factor would be needed to determine the relative contribution of each mechanism.

One possible weighting factor would be the area

tion, more accurate estimations of the number of bubbles per cell and, thus, of the area fraction of merging bubbles might be possible.

Lewis Research Center

National Aeronautics and Space Administration

Cleveland, Ohio, September 14, 1964

APPENDIX A

PROBABILITY FOR FORMATION OF BUBBLE CLUSTERS

The analysis in the text assumed the Poisson distribution of bubbles over the cells. Such an assumption implies the division of the heating surface into cells and the existence of artificial boundaries between the cells. Thus, when there are two bubbles falling into two neighboring cells but within each other's area of influence, they are not considered to be merging. Such an assumption tends to underestimate the fraction of merging bubbles. The underestimation might have been somewhat compensated for, however, by a slightly overestimated area of influence. Besides, if there are many empty cells surrounding the cells occupied by the bubbles, the cell boundary can be shifted to fit the bubbles without causing much error.

Nevertheless, a more rigorous treatment of bubble merging can be proposed by considering the probability for the clustering of bubbles.

Consider n bubbles on a heating surface A , each bubble having an area of influence a_s . The probability that another bubble will fall into the area of influence of a given bubble is a_s/A , while the probability that another bubble will not fall in the vicinity of a given bubble is $1 - a_s/A$. Therefore, the probability of having a single bubble in its area of influence is $(1 - a_s/A)^{n-1}$. The number of single bubbles is then

$$n_1 = n \left(1 - \frac{a_s}{A}\right)^{n-1} \quad (A1)$$

By the same reasoning, the probability of having only one bubble fall within the area of influence of a given bubble is

$$\frac{(n-1)!}{(n-2)!1!} \frac{a_s}{A} \left(1 - \frac{a_s}{A}\right)^{n-2}$$

The number of bubble pairs is

$$n_2 = \frac{n}{2} \frac{(n-1)!}{(n-2)!1!} \frac{a_s}{A} \left(1 - \frac{a_s}{A}\right)^{n-2} \quad (A2)$$

The general expression for the number of clusters of i bubbles is

$$n_i = \frac{n}{i} \frac{(n-1)!}{(n-i)!(i-1)!} \left(\frac{a_s}{A}\right)^{i-1} \left(1 - \frac{a_s}{A}\right)^{n-i} \quad (A3)$$

The total number of bubbles involved n should be obtained by summing all the bubbles in clusters of various sizes:

$$\begin{aligned}
\sum_{i=1}^n in_i &= \sum_{i=1}^n \frac{n(n-1)!}{(n-i)!(i-1)!} \left(\frac{a_s}{A}\right)^{i-1} \left(1 - \frac{a_s}{A}\right)^{n-i} \\
&= n \sum_{i=1}^n \frac{(n-1)!}{(n-i)!(i-1)!} \left(\frac{a_s}{A}\right)^{i-1} \left(1 - \frac{a_s}{A}\right)^{n-i} \quad (A4)
\end{aligned}$$

Since the terms within the summation sign in equation (A4) are nothing more than the binomial expression $(p + q)^{n-1}$, this term should be unity. Thus

$$\sum_{i=1}^n in_i = n$$

Hence, the fraction of bubbles that are single is, from equation (A1),

$$\mathcal{F}_1 = \frac{n_1}{n} = \left(1 - \frac{a_s}{A}\right)^{n-1} \quad (A5)$$

while the fraction of clustering bubbles is

$$\mathcal{F}_{i>1} = 1 - \mathcal{F}_1 = 1 - \left(1 - \frac{a_s}{A}\right)^{n-1} \quad (A6)$$

It is interesting to note that \mathcal{F}_1 and $\mathcal{F}_{i>1}$ are functions of the total number of bubbles involved. In other words, even if the bubble population density is the same, the clustering fraction should change when the heating area is increased, and thus the total number n will be increased. However, the functions \mathcal{F}_1 and $\mathcal{F}_{i>1}$ should reach a limit when n approaches infinity:

$$\begin{aligned}
\lim_{n \rightarrow \infty} \mathcal{F}_1 &= \lim_{n \rightarrow \infty} \left(1 - \frac{a_s}{A}\right)^{n-1} = \lim_{n \rightarrow \infty} \left[1 - (n-1) \frac{a_s}{A} + \frac{(n-1)(n-2)}{2} \left(\frac{a_s}{A}\right)^2 \right. \\
&\quad \left. - \frac{(n-1)(n-2)(n-3)}{3!} \left(\frac{a_s}{A}\right)^3 + \dots \right] \quad (A7)
\end{aligned}$$

Since $n a_s/A = \mu$ and

$$\frac{a_s}{A} = \phi_s = \frac{\mu}{n}$$

then

$$\lim_{n \rightarrow \infty} \mathcal{F}_1 = 1 - \frac{(n-1)\mu}{n} + \left[\frac{(n-1)(n-2)}{2} \left(\frac{\mu}{n} \right)^2 \right] \left[1 - \frac{(n-3)\mu}{n} \right] + \dots = 1 - \mu + \frac{\mu^2}{2!} - \frac{\mu^3}{3!} + \dots$$

Therefore,

$$\lim_{n \rightarrow \infty} \mathcal{F}_1 = 1 - \mu + \frac{\mu^2}{2!} - \frac{\mu^3}{3!} + \dots \quad (\text{A8})$$

$$\lim_{n \rightarrow \infty} \mathcal{F}_{i>1} = 1 - \mathcal{F}_1 = \mu - \frac{\mu^2}{2!} + \frac{\mu^3}{3!} + \dots \quad (\text{A9})$$

Note that $\mu = na_s/A$ is independent of the size of the heating area.

The comparison of theoretical (eq. (A5)) and experimental values of \mathcal{F}_1 is shown in figure 8.

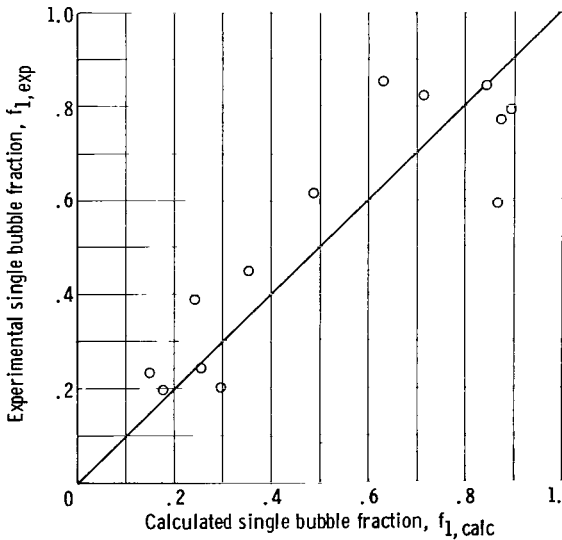


Figure 8. - Comparison of theoretical and experimental values of single bubble fractions.

To determine the area fraction covered by merging bubbles from the fraction of bubble clusters, the area occupied by each cluster a_i must be given; for example,

$$\phi_n = \sum_{i=2}^n a_i f_i \quad (\text{A10})$$

Since a_i is not readily known, however, ϕ_n cannot be obtained from \mathcal{F}_i by using equation (A10).

Of course, assumptions can be made about a_i as a function of a_s , but such assumptions involve uncertainties. Consequently, although the analysis in the test, which assumes a Poisson distribution of bubbles over the cells, is less

rigorous, it does provide the advantage of circumventing the difficulty of determining a_i .

APPENDIX B

ESTIMATION OF VARIATION ASSOCIATED WITH AVERAGE

AREA FRACTION OF MERGING BUBBLES

Consider a heating strip with area A that is divided into n_t cells, each cell being equal to the mean area of influence of a single bubble a_s .

If there are n_m cells found to be occupied by two or more bubbles and causing the coalescence of bubbles, there will be a fraction of area $\phi_m = n_m/n_t$ occupied by the merging bubbles.

When k motion picture frames were studied, it was found that there was an average value of ϕ_m

$$\phi_{m,av} = \frac{1}{k} \sum_{i=1}^k \phi_{m_i}$$

and a deviation

$$s^2 = \frac{\sum_{i=1}^k (\phi_{m_i} - \phi_{m,av})^2}{k}$$

The problem is whether or not the deviation s is theoretically expected.

If k is large (say 50 to 100), it can be assumed that $\phi_{m,av} = \mu_{\phi_m}$ is the probability of finding the merging bubble cells. Now consider the problem as that of finding the theoretical deviation σ for a binomial distribution.

$$\begin{aligned} \sigma &= \sqrt{pq/n} \\ &= \sqrt{\phi_{m,av}(1 - \phi_{m,av})/n_t} \\ n_t &= \frac{A}{a_s} = \frac{1}{\phi_{s,av}} \end{aligned}$$

or

$$\sigma = \sqrt{\frac{a_s}{A} \phi_{m,av}(1 - \phi_{m,av})} = \sqrt{\phi_{s,av} \phi_{m,av}(1 - \phi_{m,av})}$$

The comparison between s and σ is shown in table III.

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TABLE I. - EXPERIMENTAL DATA

Run	Test fluid	Bulk temperature, °F	Heat flux, q, Btu (hr)(sq ft)	Sub-cooling temperature difference between saturation and bulk, ΔT_{sub} , °F	Total number of frames studied, k	Total number of single bubbles studied in roll, h	Number of merging bubbles studied	Average instantaneous bubble population, n_{av}	Average area fraction of influence of bubble, $\phi_{\text{s,av}}$	Average area fraction of merging bubbles, $\phi_{\text{m,av}}$	Standard deviation of association with $\phi_{\text{m,av}}$	Total number of bubble sites, N
(a)												
62-12-4-1	Water	201	21,150	11	101	128	87	2.13	0.121	0.0451	0.0929	13
62-12-4-2		197	23,950	15	100	162	43	2.05	.102	.0182	.0451	10
62-12-4-3		198	32,000	14	102	172	51	2.19	.109	.0240	.0649	15
62-12-4-5		199	49,500	13	99	268	57	3.28	.138	.0402	.0936	18
62-12-4-6		196	41,500	16	102	193	35	2.24	.128	.0171	.0533	19
63-1-14-6	Methanol	132	48,300	16	96	328	57	4.01	0.143	0.0291	0.0702	18
63-2-6-1		137	92,900	11	50	139	86	4.50	.186	.115	.135	21
63-2-6-2		137	104,900	11	56	155	187	6.11	.185	.255	.225	20
63-2-6-3		140	120,700	8	47	130	202	7.06	.208	.3695	.214	30
63-2-6-4		139	135,000	9	50	92	373	9.30	.189	.535	.216	30
63-7-2-2		128	73,100	20	55	135	447	10.58	.182	.470	.183	19
63-7-8-1		111	68,400	37	70	263	196	6.56	.109	.110	.117	20
63-7-8-4		119	88,200	29	56	119	472	10.55	.121	.358	.167	26
63-7-8-5		119	82,600	29	49	124	385	10.39	.136	.327	.152	27

^aValues for methanol in this column are changed from those reported in ref. 21 because the calculation of $\phi_{\text{s,av}}$ is based on eq. (2c) in this report, while $\phi_{\text{s,av}}$ was calculated for D_{av} by using eqs. (2a) and (2b); but the changes are not large enough to alter the result.

TABLE II. - BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(a) Test fluid, water; run 62-12-4-1^a

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area frac- tion, Φ_s	Sites	Number of merg- ing bub- bles	Site center	Site width	Area frac- tion, Φ_m		Sites	Bubble center	Bubble width	Area frac- tion, Φ_s	Sites	Number of merg- ing bub- bles	Site center	Site width	Area frac- tion, Φ_m
	(b)		(b)				(b)	(b)				(b)	(b)				(b)	(b)	
0	3	5.640 6.445 7.072	0.384 0.877 0.162	0.198 0.464 0.070	0					1927	0	7.042	0.221	0.130	1	2	7.035 5.828	0.235 0.580	0.037 0.146
30	1	7.072	0.162	0.070	0					1965	1	7.047	0.211	0.119	1	2			
80	1	7.067	0.172	0.079	0					2000	1	7.060	0.185	0.091	0				
120	1	7.074	0.158	0.066	0					2029	1	7.058	0.189	0.095	1	2	5.816	0.559	0.140
160	1	7.081	0.143	0.054	1	3	5.653	1.066	0.279	2069	1	7.051	0.203	0.110	0				
195	0				1	2	6.906	0.493	0.122	2117	2	5.734	0.357	0.183	0				
240	1	7.076	0.153	0.062	0							7.067	0.171	0.078					
270	1	7.086	0.133	0.047	0					2192	1	7.062	0.181	0.087	0				
325	1	7.070	0.166	0.073	0					2237	1	7.065	0.176	0.082	0				
365	3	3.603 4.477 7.079	0.427 1.099 0.148	0.222 0.582 0.058	0					2274	2	6.003	0.304	0.246	0				
400	1	5.988	0.245	0.160	2	3	4.350	1.398	0.377			7.056	0.194	0.100					
443	2	5.698 5.998	0.179 0.220	0.085 0.129	1	2	7.074 7.067	0.157 0.171	0.010	2317	1	7.073	0.160	0.068	0				
489	1	5.705	0.176	0.082	1	2	7.056	0.193	0.012	2397	1	7.063	0.180	0.086	0				
519	1	7.068	0.169	0.076	0					2437	0	7.063	0.180	0.086	0				
564	2	5.985 7.068	0.287 0.170	0.219 0.077	0					2473	2	3.651	0.341	0.175	2	3	6.815 5.467	0.676 0.656	0.173 0.281
601	1	7.074	0.158	0.066	0					2516	0	6.030	0.296	0.233	1	2	6.919 7.052	0.467 0.201	0.027
653	2	5.709 7.080	0.343 0.146	0.176 0.057	0					2551	2	5.964	0.182	0.088	0				
685	1	7.072	0.162	0.070	0							7.057	0.192	0.098					
715	2	5.849 7.066	0.358 0.173	0.184 0.080	0					2584	1	7.053	0.200	0.106	0				
754	2	3.674 6.001	0.460 0.325	0.240 0.166	1	2	7.051	0.204	0.028	2624	1	7.066	0.174	0.081	0				
799	3	4.954 5.643 5.987	0.848 0.275 0.364	0.448 0.201 0.187	1	2	6.816	0.674	0.172	2705	1	7.071	0.164	0.072	0				
833	1	4.985	0.499	0.261	1	3	6.808	0.689	0.177	2745	2	5.720	0.149	0.059	0				
883	0				1	2	7.047	0.211	0.030			7.073	0.160	0.068					
927	4	3.685 5.712	0.398 0.156	0.206 0.065	0					2790	1	7.088	0.129	0.044	0				
										2826	2	3.700	0.405	0.210	1	2	5.892	0.492	0.121
												7.079	0.148	0.058					
										2864	1	7.074	0.157	0.066	0				
										2907	1	7.086	0.133	0.047	0				
										2953	2	5.698	0.276	0.203	0				
												7.067	0.171	0.078					
										2993	1	7.064	0.178	0.084	0				
										3025	2	5.695	0.288	0.221	0				
												6.006	0.273	0.198					

		5.979	0.089	0.021						3063	1	7.082	0.141	0.053	0				
		7.061	0.184	0.090						3103	2	5.982	0.316	0.161	0				
958	1	7.075	0.155	0.064	0							7.070	0.166	0.073					
1001	2	5.991	0.143	0.054	0					3146	2	3.657	0.534	0.280	0				
		7.065	0.176	0.082								4.060	0.161	0.069					
1033	2	5.722	0.199	0.105	0					3193	2	5.997	0.185	0.091	0				
		7.073	0.160	0.068								7.084	0.138	0.051					
1063	1	7.054	0.198	0.104	0					3228	1	5.718	0.182	0.088	1	2	7.097	0.112	0.004
1095	0				2	2	5.883	0.640	0.209	3273	0				1	2	6.800	0.706	0.181
					2	2	7.035	0.235		3313	2	5.744	0.226	0.136	1	2	6.814	0.678	0.174
1140	3	3.663	0.358	0.184	0							6.047	0.316	0.161					
		5.970	0.271	0.196						3359	1	7.106	0.094	0.024	0				
		7.072	0.162	0.070						3393	1	7.102	0.101	0.027	0				
1180	1	7.072	0.162	0.070	0					3423	1	7.110	0.086	0.020	0				
1223	3	5.687	0.242	0.156	0					3473	2	5.712	0.105	0.024	0				
		5.970	0.221	0.130								7.095	0.116	0.036					
		7.046	0.214	0.122						3513	0				1	2	7.091	0.123	0.005
1261	1	7.057	0.192	0.098	0					3548	0				1	2	7.056	0.193	0.012
1311	1	7.070	0.166	0.073	0					3593	1	5.715	0.348	0.178	1	2	6.996	0.313	0.065
1359	2	3.675	0.415	0.215	1	2	5.503	0.808	0.209	3636	0				1	2	7.056	0.193	0.012
		7.066	0.174	0.081						3674	2	5.983	0.331	0.169	0				
1411	1	7.065	0.176	0.082	0							7.086	0.134	0.048					
1441	1	7.057	0.191	0.097	0					3705	1	7.093	0.120	0.038	1	3	5.571	0.927	0.242
1486	1	7.059	0.187	0.093	0					3743	0				2	2	5.454	0.641	0.176
1521	2	3.644	0.509	0.266	1	4	6.528	1.250	0.329						2	2	7.054	0.197	
		5.615	0.231	0.142						3776	1	7.095	0.116	0.036	0				
1571	0				1	4	6.398	1.510	0.398	3820	1	7.125	0.055	0.008	0				
1600	1	4.173	0.642	0.338	1	2	7.044	0.217	0.031	3858	1	7.110	0.086	0.020	0				
1640	1	7.040	0.226	0.136	0					3906	1	7.092	0.122	0.040	0				
1690	1	7.039	0.227	0.137	0					3944	2	6.009	0.136	0.049	0				
1733	1	5.708	0.257	0.176	1	2	7.049	0.208	0.029			7.093	0.119	0.038					
1766	0				1	3	7.044	0.218	0.032	3987	3	3.796	0.356	0.183	0				
1813	1	7.057	0.191	0.097	0							5.731	0.182	0.088					
1858	2	5.995	0.258	0.177	0					4025	0	7.098	0.109	0.032	1	4	6.542	1.221	0.321
1890	2	5.713	0.295	0.232	0														

Total number of sample frames, k , 101.

Total number of single bubbles, h , 128.

Total number of merging bubbles, 87.

Average instantaneous bubble population, n_{av} , 2.13.

Average area fraction of influence of single bubble, $\phi_{s,av}$, 0.121.

Average area fraction of merging bubbles, $\phi_{m,av}$, 0.0451.

Standard deviation associated with $\phi_{m,av}$, 0.0929.

^aThis run was handled in a special manner: For each merging bubble group, the center of its width of influence is indicated. Depending on the comparison between this width of influence and the given base value of 0.20, one of two methods of computation was used in evaluating the average area fraction of merging bubbles. If the width was greater than the base value, the area of influence at each site was evaluated as one single area. If the width was less than or equal to the base value, the area of influence was evaluated by dividing the width by the number of merging bubbles at each site and summing the resulting areas.

^b3.763 movie analyzer units equal 0.75 inch; left end reading, 3.390; right end reading, 7.153.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(b) Test fluid, water; run 62-12-4-2

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area frac-tion, ϕ_s	Sites	Number of merging bub-bles	Site center	Site width	Area frac-tion, ϕ_m		Sites	Bubble center	Bubble width	Area frac-tion, ϕ_s	Sites	Number of merging bub-bles	Site center	Site width	Area frac-tion, ϕ_m
		(a)	(a)				(a)	(a)				(a)	(a)			(a)	(a)		
0	2	5.216	0.170	0.074	0					1965	2	4.977	0.216	0.120	0				
30	3	6.379	0.130	0.043								6.387	0.084	0.018					
		4.153	0.386	0.195	2	2	2.661	0.375	0.202	2000	1	4.288	0.499	0.256	0				
		6.187	0.136	0.047			2.833	0.217		2029	3	4.295	0.289	0.214	0				
		6.282	0.106	0.029		2	4.839	0.315				4.954	0.193	0.095					
80	2	4.934	0.382	0.193	0							6.413	0.065	0.011					
		6.396	0.121	0.038						2069	2	2.937	0.319	0.261	0				
		6.324	0.164	0.069	0							6.352	0.104	0.028					
120	1	6.324	0.164	0.069	0					2117	2	5.224	0.185	0.088	0				
160	1	5.096	0.082	0.017	1	2	6.160	0.129	0.018			6.421	0.077	0.015					
195	2	5.190	0.176	0.079	0					2152	1	6.413	0.088	0.020	0				
		6.393	0.084	0.018						2192	1	6.192	0.143	0.052	1	2	4.875	0.294	0.089
240	1	4.496	0.326	0.163	1	2	6.212	0.100	0.011	2274	1	6.265	0.110	0.031	1	2	5.137	0.230	
270	3	2.895	0.148	0.056	0														
		5.216	0.158	0.064								2.905	0.155	0.062	0				
		6.405	0.060	0.009								6.121	0.070	0.013					
325	1	4.254	0.499	0.256	0							6.272	0.177	0.080					
365	2	4.229	0.341	0.171	0							6.401	0.071	0.013					
400	1	6.405	0.092	0.022						2347	1	6.425	0.070	0.013	0				
		6.220	0.247	0.156	1	2	4.858	0.240	0.085	2397	1	6.344	0.185	0.088	0				
							5.115	0.274		2437	1	6.316	0.176	0.079	0				
443	3	4.948	0.210	0.113	0					2473	2	5.966	0.351	0.177	0				
		5.230	0.288	0.213								6.289	0.258	0.171					
		6.349	0.148	0.056						2516	2	5.215	0.137	0.048	0				
489	1	6.268	0.118	0.036	1	2	4.850	0.240	0.103			6.425	0.062	0.010					
							5.130	0.321		2551	3	2.922	0.214	0.117	0				
519	1	6.340	0.109	0.030	0							4.945	0.083	0.018					
564	1	6.289	0.250	0.160	0							6.387	0.110	0.031					
601	1	6.293	0.122	0.038	1	2	4.992	0.383	0.134	2584	2	5.237	0.210	0.113	0				
653	2	2.846	0.348	0.175	1	2	5.191	0.271				6.399	0.091	0.021					
		5.105	0.277	0.197			6.238	0.126	0.014	2624	3	4.242	0.636	0.328	0				
		5.862	1.246	0.648	0		6.325	0.080				4.950	0.245	0.154					
685	1	5.862	1.246	0.648	0							6.384	0.083	0.018					
715	1	6.029	0.082	0.017	0					2673	2	4.295	0.322	0.161	0				
754	1	6.337	0.202	0.105	0							6.341	0.121	0.038					
799	1	6.235	0.112	0.032	1	2	4.176	0.597	0.157	2705	1	4.254	0.532	0.273	0				
							4.162	0.116		2790	4	2.913	0.102	0.027	0				
833	1	6.307	0.125	0.040	1	2	4.146	0.458	0.128			4.670	0.299	0.229					
							4.128	0.173				5.238	0.208	0.111					
												6.418	0.077	0.015					
883	2	4.648	0.614	0.317	0					2826	3	4.921	0.233	0.139	0				
927	1	6.392	0.185	0.088								5.228	0.175	0.079					
		4.703	0.366	0.185	0							6.406	0.074	0.014					

958	4	2.921	0.309	0.245	0					2864	2	4.686	0.419	0.213	0				
		3.689	0.379	0.192								6.404	0.089	0.020					
		4.220	0.554	0.285						2907	1	6.387	0.100	0.026	0				
		6.382	0.079	0.016						2953	1	6.364	0.071	0.013	0				
1001	1	4.298	0.249	0.159	0					2993	1	6.370	0.078	0.016	0				
1033	2	5.231	0.249	0.159	0					3025	2	2.928	0.430	0.219	0				
		6.398	0.077	0.015								6.359	0.111	0.032					
1063	2	4.963	0.126	0.041	0					3103	2	5.229	0.120	0.037	0				
		6.375	0.101	0.026								6.430	0.057	0.008					
1095	1	5.139	0.164	0.069	1	2	6.246	0.125	0.014	3146	4	4.941	0.233	0.139	0				
							6.332	0.078				5.217	0.140	0.050					
1140	1	6.398	0.081	0.017	0							5.954	0.235	0.142					
1180	2	4.959	0.403	0.205	0							6.375	0.071	0.013					
		6.388	0.107	0.029								2.909	0.443	0.226	0				
1261	0				2	2	4.828	0.381	0.121	3193	1	6.387	0.063	0.010	0				
							5.108	0.178		3228	1	6.381	0.076	0.015	0				
						2	6.206	0.105		3273	1	6.381	0.076	0.015	0				
							6.302	0.107		3313	4	2.870	0.440	0.224	0				
												5.201	0.152	0.059					
1311	1	5.211	0.093	0.022	0							5.685	0.771	0.399					
1359	1	6.252	0.100	0.026	1	2	4.838	0.341	0.085			6.256	0.161	0.066					
							4.871	0.138		3359	1	6.413	0.102	0.027	0				
1411	3	4.250	0.234	0.140	0					3393	4	2.950	0.354	0.178	0				
		5.204	0.196	0.098								4.957	0.193	0.095					
		6.366	0.092	0.022								5.226	0.136	0.047					
1441	2	2.876	0.452	0.231	0							6.421	0.083	0.018					
		6.344	0.112	0.032						3473	2	4.190	0.552	0.284	1	2	4.984	0.466	0.126
1486	1	3.916	2.350	1.225	1	3	5.894	0.370	0.107			6.301	0.085	0.019			5.230	0.153	
							5.866	0.089		3513	3	3.438	0.720	0.372	0				
							6.135	0.176				4.337	0.402	0.204					
1521	1	6.344	0.126	0.041	0							6.351	0.128	0.042					
1571	1	6.363	0.070	0.013	0					3548	3	4.222	0.511	0.262	0				
1600	1	6.317	0.114	0.033	0							4.977	0.374	0.189					
1640	2	5.211	0.138	0.049	0							6.439	0.077	0.015					
		6.275	0.134	0.046						3593	1	6.425	0.068	0.012	0				
1690	2	4.254	0.260	0.173	0					3636	2	4.838	0.111	0.032	1	2	4.569	0.524	0.136
		4.613	0.306	0.240								6.278	0.108	0.030			4.558	0.112	
1733	1	6.319	0.095	0.023	0					3674	1	6.346	0.089	0.020	1	2	4.168	0.356	0.170
1766	1	2.798	0.091	0.021	1	2	6.234	0.073	0.008							4.545	0.399		
							6.312	0.083		3743	1	6.288	0.166	0.071	0				
1813	1	6.338	0.102	0.027	0					3776	1	6.014	0.265	0.180	0				
1858	2	5.217	0.117	0.035	0					3820	3	4.954	0.139	0.050	0				
		6.325	0.090	0.021								5.228	0.252	0.163					
1890	3	4.947	0.047	0.006	0							6.442	0.074	0.014					
		6.296	0.120	0.037						3858	1	6.424	0.071	0.013	0				
		6.434	0.068	0.012						3906	2	5.247	0.185	0.088	0				
1927	2	5.225	0.104	0.028	0							6.394	0.072	0.013					
		6.360	0.100	0.026						3944	1	6.357	0.119	0.036	0				

Total number of sample frames, k, 100.
 Total number of single bubbles, h, 162.
 Total number of merging bubbles, 43.
 Average instantaneous bubble population, n_{av} , 2.05.
 Average area fraction of influence of single bubble, $\phi_{s,av}$, 0.102.
 Average area fraction of merging bubbles, $\phi_{m,av}$, 0.0182.
 Standard deviation associated with $\phi_{m,av}$, 0.0451.

^a3.835 movie analyzer units equal 0.75 inch; left end reading, 2.650; right end reading 6.485.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(c) Test fluid, water; run 62-12-4-3^a

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area frac-tion, φ_s	Sites	Number of merging bub-bles	Site center	Site width	Area frac-tion, φ_m		Sites	Bubble center	Bubble width	Area frac-tion, φ_s	Sites	Number of merging bub-bles	Site center	Site width	Area frac-tion, φ_m
		(b)	(b)				(b)	(b)					(b)	(b)				(b)	(b)
0	1	6.873	0.080	0.016	0							4.741	0.412	0.206					
30	1	6.840	0.109	0.030	0							7.000	0.103	0.026					
80	2	5.401	0.166	0.069	0					2274	2	4.228	0.655	0.334	0				
		6.863	0.157	0.062								6.999	0.112	0.031					
120	2	4.606	0.255	0.162	1	2	5.229	0.781	0.175	2317	1	4.208	0.390	0.195	0				
		6.895	0.113	0.032						2347	2	3.425	0.414	0.208	0				
160	2	6.189	0.391	0.195	0							6.972	0.102	0.026					
		6.889	0.136	0.046						2397	3	3.259	0.192	0.092	0				
195	1	6.883	0.100	0.025	0							5.776	0.152	0.058					
240	1	3.170	0.174	0.076	0							7.009	0.075	0.014					
270	1	6.888	0.132	0.043	0					2437	4	3.411	0.347	0.172	0				
325	2	4.477	0.313	0.245	0							5.476	0.280	0.196					
		5.421	0.299	0.223								5.787	0.225	0.126					
365	1	6.935	0.074	0.014	1	3	6.307	0.656	0.090			6.984	0.074	0.014					
400	2	3.331	0.078	0.015	0					2473	1	6.970	0.091	0.021	1	4	6.127	1.497	0.329
		6.925	0.102	0.026	0					2624	2	6.868	0.069	0.012	0				
489	1	6.928	0.103	0.026	0							7.007	0.055	0.008					
519	2	4.031	0.321	0.257	0					2673	3	4.569	0.714	0.364	0				
		6.875	0.210	0.110								5.534	0.254	0.161					
564	1	6.876	0.207	0.107	1	4	5.361	1.008	0.159			6.986	0.100	0.025					
601	2	4.494	0.139	0.048	0					2705	4	3.436	0.332	0.164	0				
		6.902	0.155	0.060								4.609	0.087	0.019					
653	1	6.924	0.112	0.031	0							5.810	0.157	0.062					
685	1	5.750	0.086	0.018	1	2	6.901	0.177	0.010			6.982	0.094	0.022					
715	1	4.511	0.273	0.186	2	2	3.332	0.342	0.072	2745	4	3.245	0.181	0.082	1	2	5.673	0.512	0.082
					2	2	6.854	0.280				3.909	0.657	0.335					
754	3	3.833	0.218	0.119	2	2	4.458	0.189	0.025			4.626	0.382	0.191					
		5.468	0.291	0.211	2	2	6.897	0.214				7.003	0.097	0.023					
		5.744	0.099	0.024						2790	3	3.862	0.351	0.174	0				
799	2	6.836	0.101	0.025	0							4.572	0.189	0.089					
		6.962	0.095	0.023								6.995	0.127	0.040					
833	2	5.764	0.136	0.046	0					2826	3	4.670	0.188	0.088	0				
		6.968	0.097	0.023								5.211	0.498	0.252					
883	2	5.484	0.249	0.155	0							7.017	0.111	0.031					
		6.965	0.104	0.027						2864	2	5.328	0.333	0.164	0				
958	2	4.547	0.098	0.024	0							6.973	0.128	0.041					
		5.784	0.116	0.034						2907	4	3.278	0.232	0.134	0				
1001	1	6.609	0.303	0.224	0							4.572	0.168	0.070					
1033	1	4.208	0.663	0.338	1	2	6.958	0.133	0.006			5.801	0.149	0.055					
1063	3	4.202	0.432	0.217	0							7.019	0.087	0.019					
		5.207	0.582	0.290						2953	4	3.407	0.371	0.185	0				
		6.956	0.062	0.010								4.227	0.315	0.248					
1095	1	5.167	0.393	0.196	1	2	6.924	0.196	0.012			5.809	0.193	0.091					
1180	1	6.888	0.263	0.173	0							6.981	0.118	0.035					
1223	1	6.994	0.081	0.016	1	2	6.491	0.850	0.195	2993	1	6.958	0.142	0.050	0				

1261	1	6.930	0.073	0.013	0					3025	3	5.519	0.272	0.185	0				
1311	1	6.948	0.073	0.013	0							6.608	0.514	0.260					
1359	3	3.411	0.245	0.150	1	2	5.565	0.391	0.048			7.015	0.099	0.024					
		5.817	0.071	0.013						3063	2	6.614	0.365	0.181	0				
		6.958	0.077	0.015								6.988	0.154	0.059					
1411	2	5.779	0.142	0.050	1	2	5.251	0.832	0.190	3146	1	7.031	0.079	0.016	0				
		7.011	0.065	0.011						3193	2	4.555	0.336	0.166	1	2	5.554	0.447	0.062
1441	3	3.885	0.717	0.366	0							6.949	0.125	0.039					
		5.790	0.066	0.011						3228	2	5.804	0.284	0.201	0				
		6.934	0.109	0.030								7.026	0.096	0.023					
1486	3	3.778	0.422	0.212	0					3273	1	6.965	0.143	0.051	0				
		4.719	0.811	0.415						3313	1	6.989	0.091	0.021	1	2	5.295	0.944	0.222
		6.928	0.124	0.038						3359	2	4.555	0.254	0.161	0				
1521	2	4.732	0.319	0.254	0							5.113	0.304	0.231					
		6.931	0.081	0.016						3393	1	4.499	0.289	0.209	0				
1571	1	3.400	0.289	0.209	0					3423	0				1	3	6.446	1.232	0.280
1600	2	5.793	0.228	0.130	0					3473	2	5.489	0.129	0.042	0				
		6.929	0.153	0.058								6.990	0.079	0.016					
1640	1	4.226	0.597	0.303	1	3	6.717	0.679	0.096	3513	4	3.297	0.270	0.182	0				
1690	4	3.275	0.198	0.098	0							3.885	0.626	0.319					
		4.203	0.419	0.210								5.486	0.150	0.056					
		5.808	0.260	0.169								6.972	0.084	0.018					
		7.024	0.076	0.014						3548	4	3.809	0.157	0.062	0				
1733	1	5.584	0.314	0.246	0							4.527	0.604	0.307					
1766	1	7.020	0.075	0.014	0							5.495	0.218	0.119					
1813	1	5.511	0.156	0.061	0							6.969	0.099	0.024					
1858	2	3.304	0.248	0.154	0					3593	2	4.548	0.353	0.175	0				
		7.001	0.075	0.014								6.968	0.086	0.018					
1890	1	7.022	0.083	0.017	0					3743	2	3.220	0.139	0.048	0				
1965	1	6.968	0.082	0.017	1	2	3.727	1.095	0.264			4.169	0.571	0.290					
2000	3	3.866	0.379	0.189	0					3776	2	4.175	0.386	0.193	0				
		5.504	0.180	0.081								6.954	0.099	0.024					
		6.980	0.091	0.021						3820	3	4.558	0.099	0.024	0				
2029	3	3.931	0.418	0.210	0							5.691	0.088	0.019					
		5.789	0.177	0.078								6.993	0.076	0.014					
		6.996	0.116	0.034						3906	4	5.464	0.185	0.085	0				
2069	3	5.172	0.148	0.055	1	2	5.734	0.644	0.129			5.768	0.272	0.185					
		6.218	0.240	0.144								6.584	0.307	0.235					
		6.901	0.145	0.052								6.967	0.127	0.040					
2152	1	6.992	0.063	0.010	1	2	6.905	0.077	0.002	3944	1	3.247	0.200	0.100	0				
2192	1	4.748	0.763	0.390	0					3987	1	4.536	0.395	0.197	0				
2237	3	3.418	0.364	0.181	0					4025	1	6.923	0.122	0.037	0				

Total number of sample frames, k, 102.

Total number of single bubbles, h, 172.

Total number of merging bubbles, 51.

Average instantaneous bubble population, n_{av} , 2.19.

Average area fraction of influence of single bubble, $\phi_{s,av}$, 0.109.

Average area fraction of merging bubbles, $\phi_{m,av}$, 0.0240.

Standard deviation associated with $\phi_{m,av}$, 0.0649.

^aThis run was handled in a special manner: For each merging bubble group, the center of its width of influence is indicated. Depending on the comparison between this width of influence and the given base value of 100.00, one of two methods of computation was used in evaluating the average area fraction of merging bubbles. If the width was greater than the base value, the area of influence at each site was evaluated as one single area. If the width was less than or equal to the base value, the area of influence was evaluated by dividing the width by the number of merging bubbles at each site and summing the resulting areas.

^b3.886 movie analyzer units equal 0.75 inch; left end reading, 3.146; right end reading, 7.032.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(d) Test fluid, water; run 62-12-4-5

Frame	Single bubbles				Merging bubbles				Frame	Single bubbles				Merging bubbles								
	Sites	Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width		Area fraction, φ_m	Sites	Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m			
		(a)	(a)				(a)	(a)				(a)	(a)			(a)	(a)					
0	5	3.324	0.387	0.192	0				2000	1	6.865	0.192	0.091	0								
		4.492	0.316	0.247																		
		5.448	0.214	0.113																		
		5.746	0.253	0.158																		
		6.922	0.135	0.045																		
30	4	3.352	0.541	0.273	0				2029	5	3.315	0.407	0.203	0								
		4.519	0.348	0.171																		
		5.178	0.243	0.146																		
		6.931	0.117	0.034																		
		3.891	0.303	0.227																		
80	3	5.728	0.298	0.219	0				2069	1	5.450	0.257	0.163	0								
		6.852	0.133	0.044																		
		3.750	0.548	0.276																		
		6.448	0.622	0.315																		
		6.854	0.143	0.051																		
160	3	3.092	0.173	0.074	1	2	3.081	0.140	0.034	2152	3	3.839	0.224	0.124	0							
		3.271	0.264	0.172			3.198	0.188	4.536			0.377	0.187									
		4.397	0.428	0.214			5.623	0.151	6.534			0.185	0.085									
		6.851	0.144	0.051					6.796			0.139	0.048	1		2	5.409	0.278	0.062			
		4.404	0.560	0.283													5.623	0.151				
240	2	6.821	0.202	0.101	1	3	5.006	0.572	0.104	2237	0				1	2	3.146	0.273	0.108			
							5.456	0.329	5.623			0.151								3.300	0.316	
							5.725	0.209												5.369	0.294	0.068
																				5.648	0.155	
																				6.433	0.635	0.176
270	3	3.160	0.166	0.068	0				2274	1	5.022	0.193	0.092	1	2	5.369	0.294	0.068				
		4.582	0.341	0.168															5.648	0.155		
		6.960	0.049	0.006															6.433	0.635	0.176	
		3.248	0.186	0.085																		
		5.367	0.170	0.071																		
325	2				1	4	5.702	0.361	0.276	2317	3	3.073	0.134	0.044	1	2	5.369	0.294	0.068			
							6.083	0.401	3.073			0.134	0.044									
							6.501	0.435	4.416			0.474	0.238									
							6.779	0.120	5.368			0.221	0.121									
									5.452			0.268	0.177	0								
365	3				1	4				2347	3	5.771	0.260	0.167	0							
									6.532			0.784	0.399									
									6.118			0.497	0.250	0								
									6.904			0.131	0.042									
									3.870			0.551	0.278	0								
400	4				1	4				2437	1	3.797	0.271	0.181	0							
									4.494			0.455	0.228									
									5.152			0.695	0.353									
									4.490			0.290	0.208	0								
									5.052			0.352	0.174									
443	3				0				2516	5	5.746	0.145	0.052	0								
								6.538			0.160	0.063										
								6.921			0.097	0.023										
								3.541			0.342	0.168	0									
								6.486			0.236	0.138										
489	2				0				2551	3	6.935	0.069	0.012	0								
								6.935			0.069	0.012										
								3.260			0.302	0.225	0									
								5.754			0.181	0.081										
								6.517			0.186	0.085										
519	1				1	2				2584	4	6.953	0.058	0.008	0							
									6.935			0.093	0.021									
									5.435			0.108	0.029	0								
									6.830			0.137	0.046									
									5.436			0.083	0.017	0								
601	4				0				2624	1	6.003	0.543	0.274	0								
								6.546			0.542	0.273										
								3.769			0.246	0.150	0									
								4.470			0.556	0.281										
								6.518			0.077	0.015										
653	1				0				2673	2	6.914	0.083	0.017	0								
								3.310			0.496	0.249	0									
								3.801			0.200	0.099										
								4.493			0.230	0.131										
								5.427			0.302	0.225										
685	1				1	2				2745	3	5.723	0.189	0.088	0							
									6.924			0.076	0.014									
									3.171			0.218	0.117									
									4.458			0.390	0.194									
									5.429			0.443	0.222									
715	2				0				2790	4	5.793	0.284	0.199	0								
								6.901			0.122	0.037										
								6.904			0.116	0.033	0									
								3.127			0.130	0.042	0									
								4.499			0.390	0.194										
754	4				0				2826	6	5.117	0.242	0.145	0								
								6.764			0.137	0.046										
799	5				0				2864	5				0								
833	3				0				2907	1				0								
883	2				1	2			2953	4				0								
927	4				0									0								

1001	3	6.919	0.098	0.024	1	2	6.424	0.506	0.166	2993	1	3.209	0.400	0.199	1	2	4.218	0.724	0.326
		4.386	0.283	0.198			6.700	0.274		3025	3	3.823	0.357	0.176	0		4.883	0.606	
		5.357	0.244	0.147								4.196	0.389	0.193					
		5.637	0.185	0.085								4.995	0.301	0.224					
1033	4	3.248	0.281	0.195	1	3	5.362	0.265	0.181	3063	2	3.841	0.224	0.124	0				
		3.738	0.588	0.297			5.619	0.248				4.475	0.218	0.117					
		4.429	0.259	0.166			5.960	0.434		3103	1	3.161	0.179	0.079	0				
		6.539	0.326	0.160						3146	4	4.489	0.572	0.289	0				
1063	3	3.177	0.217	0.116	0							6.091	0.547	0.276					
		3.781	0.262	0.170								6.574	0.419	0.209					
		5.452	0.179	0.079								6.895	0.119	0.035					
1095	3	3.103	0.069	0.012	0					3193	3	3.843	0.504	0.254	0				
		5.744	0.297	0.218								4.469	0.243	0.146					
		6.891	0.157	0.061								5.739	0.187	0.086					
1140	3	4.596	0.240	0.142	0					3228	3	3.815	0.317	0.248	0				
		5.448	0.194	0.093								5.735	0.224	0.124					
		5.748	0.101	0.025								6.823	0.167	0.069					
1180	3	3.301	0.311	0.239	0					3273	5	4.459	0.250	0.154	0				
		6.732	0.120	0.036								5.114	0.363	0.179					
		6.921	0.109	0.029								5.425	0.162	0.065					
1223	3	4.079	0.766	0.389	1	2	3.048	0.111	0.042			5.751	0.210	0.109					
		5.357	0.109	0.023			3.221	0.235				6.928	0.079	0.015					
		5.650	0.114	0.032						3313	3	3.318	0.364	0.180	0				
1261	2	5.241	0.272	0.183	1	4	5.573	0.247	0.256			6.447	0.377	0.187					
		6.823	0.194	0.093			5.971	0.549				6.937	0.077	0.015					
							6.245	0.149		3359	3	6.035	0.403	0.201	0				
							6.493	0.346				6.476	0.240	0.142					
1311	4	3.808	0.362	0.179	0							6.889	0.174	0.075					
		4.496	0.282	0.197						3393	2	3.335	0.529	0.267	0				
		5.468	0.226	0.126								6.923	0.105	0.027					
		5.732	0.135	0.045						3473	1	5.707	0.206	0.105	0				
1359	2	3.809	0.318	0.250	0					3513	4	4.468	0.118	0.034	0				
		4.440	0.380	0.188								5.124	0.187	0.086					
1411	3	5.059	0.395	0.196	0							5.420	0.287	0.204					
		5.442	0.371	0.184								5.713	0.151	0.056					
		6.932	0.080	0.016						3548	4	3.840	0.130	0.042	0				
1486	2	5.705	0.154	0.059	0							5.742	0.244	0.147					
		6.509	0.597	0.302								6.456	0.391	0.194					
1521	3	3.822	0.281	0.195	0							6.842	0.204	0.103					
		5.723	0.235	0.136						3593	3	3.832	0.233	0.134	0				
		6.479	0.211	0.110								5.747	0.122	0.037					
		4.508	0.614	0.311	0							6.579	0.199	0.098					
1571	2	6.790	0.164	0.066						3636	6	3.307	0.277	0.190	0				
		4.493	0.395	0.196	0							4.496	0.464	0.233					
1600	1	6.707	0.166	0.068	3	2	3.129	0.251	0.529			5.377	0.391	0.194					
1640	1						3.532	0.555				5.699	0.252	0.157					
							4.069	0.355				6.126	0.602	0.304					
							4.414	0.335				6.910	0.146	0.053					
							5.386	0.123		3674	1	6.745	0.189	0.088	2	2	4.009	0.449	0.354
							6.058	0.567									4.450	0.433	
																	5.049	0.472	
																	5.412	0.255	
1733	1	3.319	0.210	0.109	0												4.212	0.164	0.036
1766	3	3.824	0.114	0.032	0					3705	2	3.234	0.319	0.251	1	2	4.383	0.179	
		4.497	0.287	0.204								6.858	0.145	0.052					
		5.454	0.436	0.218						3743	2	3.144	0.180	0.080	0				
1813	4	3.812	0.105	0.027	0							3.824	0.631	0.319					
		5.057	0.368	0.182						3776	5	3.304	0.254	0.159	0				
		5.415	0.348	0.171								3.795	0.221	0.121					
		6.881	0.131	0.042								4.467	0.153	0.058					
1858	3	3.241	0.231	0.132	1	2	4.057	0.322	0.130			5.436	0.179	0.079					
		5.670	0.223	0.123			4.428	0.328				6.921	0.117	0.034					
		6.887	0.074	0.014						3820	2	5.433	0.191	0.090	0				
1890	5	4.266	0.231	0.132	0							6.860	0.136	0.046					
		5.444	0.192	0.091						3858	1	6.823	0.149	0.055	1	2	4.346	0.292	0.132
		5.721	0.132	0.043													4.674	0.365	
		6.530	0.244	0.147															
		6.927	0.084	0.017						3906	2	3.280	0.238	0.140	0				
1927	2	5.303	0.269	0.179	1	2	5.647	0.324	0.169	3944	2	5.708	0.206	0.105					
		6.846	0.126	0.039			6.034	0.450				5.709	0.125	0.039	0				
		3.820	0.345	0.170	0					3987	5	6.539	0.110	0.030					
1965	5	4.481	0.281	0.195								3.327	0.404	0.201	0				
		5.473	0.347	0.171								5.063	0.219	0.119					
		6.087	0.168	0.070								5.456	0.255	0.161					
		6.920	0.097	0.023								5.756	0.193	0.092					
												6.929	0.110	0.030					

Total number of sample frames, k , 99.

Total number of single bubbles, h , 266.

Total number of merging bubbles, 57.

Average instantaneous bubble population, n_{av} , 3.28.

Average area fraction of influence of single bubble, $\phi_{s,av}$, 0.136.

Average area fraction of merging bubbles, $\phi_{m,av}$, 0.0402.

Standard deviation associated with $\phi_{m,av}$, 0.0936.

^a3.906 movie analyzer units equal 0.75 inch; left end reading, 3.070; right end reading, 6.976.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(e) Test fluid, water; run 62-12-4-6

Frame	Sites	Single bubbles			Merging bubbles					Frame	Sites	Single bubbles			Merging bubbles				
		Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m			Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m
		(a)	(a)				(a)	(a)				(a)	(a)				(a)	(a)	
0	1	6.886	0.064	0.010	0					2000	1	6.895	0.128	0.040	0				
30	0				1	2	6.712	0.116	0.014	2029	1	3.769	0.606	0.306	0				
							6.782	0.097		2069	1	3.692	0.285	0.200	2		5.432	0.204	0.296
80	2	3.651	0.297	0.217	0												5.651	0.234	
		6.824	0.144	0.051													5.938	0.341	
120	3	3.089	0.204	0.102	0												6.447	0.677	
		5.378	0.222	0.121						2117	2	4.414	0.383	0.190	0				
		6.890	0.069	0.012								5.378	0.191	0.090					
160	1	6.877	0.095	0.022	0					2192	3	3.098	0.146	0.052	0				
195	2	3.161	0.449	0.224	0							3.299	0.256	0.161					
		6.753	0.097	0.023								5.080	0.324	0.258					
240	1	6.835	0.103	0.026	0					2237	1	6.841	0.115	0.033	0				
270	1	6.878	0.107	0.028	0					2274	2	4.090	0.152	0.057	0				
325	1	6.343	0.250	0.154	1	2	5.258	0.238	0.053			5.684	0.116	0.033					
							5.528	0.172		2317	4	5.068	0.483	0.242	0				
365	8	3.221	0.308	0.234	0							5.427	0.234	0.135					
		3.626	0.502	0.252								5.712	0.162	0.065					
		4.114	0.475	0.238								6.925	0.066	0.011					
		5.363	0.343	0.168						2347	3	3.253	0.198	0.097	0				
		5.685	0.174	0.075								5.389	0.199	0.098					
		5.984	0.424	0.211								5.697	0.271	0.181					
		6.402	0.326	0.262						2397	1	3.145	0.238	0.139	0				
		6.816	0.179	0.079						2437	1	3.773	0.229	0.129	0				
400	3	3.065	0.166	0.068	0					2473	1	5.385	0.167	0.069	0				
		6.694	0.126	0.039						2516	4	3.297	0.435	0.217	0				
		6.814	0.114	0.032								5.389	0.271	0.181					
443	2	3.241	0.412	0.205	0							5.680	0.311	0.238					
		6.876	0.072	0.013								6.743	0.134	0.044					
489	1	3.245	0.465	0.233	0					2551	3	5.354	0.294	0.213	0				
519	1	5.670	0.099	0.024	0							5.674	0.346	0.170					
564	2	6.419	0.297	0.217	0							6.458	0.506	0.254					
		6.870	0.093	0.021						2584	4	4.468	0.325	0.260	0				
601	1	4.417	0.410	0.204	0							5.403	0.167	0.069					
653	2	4.537	0.519	0.261	1	2	5.379	0.130	0.190			6.498	0.178	0.078					
		6.721	0.190	0.089			5.870	0.729				6.934	0.075	0.014					
685	2	6.012	0.235	0.136	0					2624	2	3.055	0.207	0.105	1	2	3.155	0.378	0.232
		6.845	0.150	0.055								4.601	0.450	0.225			3.703	0.615	
715	2	4.450	0.354	0.174	0					2673	1	3.729	0.331	0.162	0				
		5.398	0.309	0.235						2790	1	6.921	0.099	0.024	0				
799	2	4.123	0.520	0.261	0					2826	1	5.411	0.315	0.244	0				
		6.934	0.070	0.012						2864	1	4.373	0.316	0.246	1	2	3.027	0.158	0.040
833	1	6.918	0.102	0.026	0												3.163	0.199	
883	2	4.305	0.346	0.170	2	3	4.669	0.288	0.181	2907	2	6.385	0.432	0.215	1	2	5.076	0.341	0.118
		6.428	0.226	0.126			4.881	0.136				6.788	0.115	0.033			5.385	0.277	
							5.186	0.474		2953	3	3.236	0.140	0.048	0				
							6.744	0.083				4.436	0.168	0.069					
							6.823	0.074				6.471	0.229	0.129					
927	2	3.279	0.238	0.139	0					2993	2	5.390	0.188	0.087	0				
		6.849	0.135	0.045								5.683	0.126	0.039					

1001	1	5.692	0.229	0.129	0					3025	3	5.388	0.110	0.030	0				
1033	3	3.014	0.143	0.050	1	2	5.300	0.198	0.072			5.682	0.115	0.033					
		6.377	0.548	0.276			5.589	0.279				5.988	0.108	0.029					
		6.803	0.102	0.026								3.195	0.215	0.114	1	2	4.061	0.394	0.122
1063	6	3.265	0.263	0.170	0							5.333	0.165	0.067			4.427	0.237	
		3.804	0.345	0.170								3.129	0.213	0.112	0				
		4.445	0.179	0.079								4.084	0.300	0.222					
		5.105	0.442	0.221								5.098	0.333	0.163					
		5.699	0.240	0.142								5.430	0.219	0.118					
		6.514	0.208	0.107								3.767	0.263	0.170	0				
1095	3	3.827	0.198	0.097	0							4.429	0.268	0.177					
		6.510	0.103	0.026								5.052	0.323	0.257					
		6.923	0.091	0.020								5.396	0.268	0.177					
1140	2	4.335	0.273	0.184	2	2	3.046	0.229	0.163			5.689	0.087	0.019					
		6.803	0.132	0.043								6.498	0.200	0.098					
						3	3.213	0.230				3.788	0.114	0.032	0				
							5.246	0.137				6.887	0.121	0.036					
							5.529	0.225				3393	1	6.844	0.101	0.025	0		
							5.881	0.314				3423	2	3.267	0.352	0.173	0		
1180	2	4.096	0.629	0.318	0							4.460	0.424	0.211					
		6.915	0.086	0.018								3513	1	5.463	0.093	0.021	0		
1223	4	3.789	0.224	0.124	0							3548	2	3.749	0.786	0.399	0		
		5.391	0.215	0.114								6.873	0.143	0.050					
		6.452	0.080	0.016								3593	2	5.058	0.355	0.175	0		
		6.937	0.064	0.010								6.480	0.276	0.188					
1261	3	5.413	0.261	0.168	0							3636	3	4.438	0.203	0.101	0		
		6.632	0.088	0.019								6.011	0.583	0.294					
		6.920	0.097	0.023								6.792	0.312	0.240					
1311	1	5.386	0.291	0.208	0							3674	1	6.874	0.094	0.022	0		
1359	3	3.309	0.551	0.277	0							3705	2	4.653	0.197	0.096	0		
		3.820	0.470	0.235								5.408	0.308	0.234					
		5.118	0.601	0.303								3743	4	3.129	0.175	0.075	0		
1411	1	6.445	0.600	0.303	0							3.331	0.229	0.129					
1441	1	6.485	0.258	0.164	0							4.677	0.237	0.138					
1486	2	5.670	0.107	0.028	0							5.411	0.284	0.199					
		6.852	0.072	0.013								4.478	0.187	0.086	0				
1521	3	3.743	0.163	0.065	0							4.717	0.290	0.207					
		5.375	0.196	0.095								6.943	0.070	0.012					
		5.651	0.162	0.065								3820	1	6.908	0.119	0.035	0		
1640	2	3.101	0.198	0.097	1	3	5.198	0.204	0.196			3858	1	5.443	0.323	0.257	0		
		4.284	0.262	0.169			5.508	0.317				3906	4	4.105	0.594	0.300	0		
							5.900	0.466				4.524	0.244	0.147					
1733	1	6.884	0.100	0.025	0							6.496	0.545	0.274					
1766	2	3.229	0.328	0.160	0							6.876	0.079	0.015					
		6.474	0.305	0.229								4.125	0.373	0.184	0				
1813	1	6.866	0.106	0.028	0							6.529	0.183	0.082					
1858	2	3.150	0.417	0.208	1	2	5.305	0.242	0.063			3944	2	3.281	0.130	0.042	0		
		6.774	0.141	0.049			5.583	0.209				3987	3	5.385	0.202	0.100			
1890	6	3.207	0.271	0.181	0							5.690	0.152	0.057					
		3.751	0.313	0.241								3.794	0.292	0.210	0				
		4.391	0.200	0.098								4.441	0.244	0.147					
		5.055	0.403	0.200								5.388	0.265	0.173					
		5.401	0.288	0.204								5.699	0.249	0.153					
		5.691	0.188	0.087								6.920	0.086	0.018					
1927	1	6.874	0.112	0.031	0														
1965	1	6.800	0.137	0.046	0														

Total number of sample frames, k, 102.
 Total number of single bubbles, h, 193.
 Total number of merging bubbles, 35.
 Average instantaneous bubble population, n_{av} , 2.24.
 Average area fraction of influence of single bubble, $\phi_{s,av}$, 0.128.
 Average area fraction of merging bubbles, $\phi_{m,av}$, 0.0171.
 Standard deviation associated with $\phi_{m,av}$, 0.0533.

^a3.913 movie analyzer units equal 0.75 inch; left end reading, 3.032; right end reading, 6.945.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(f) Test fluid, methanol; run 63-1-14-6

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m		Sites	Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m
		(a)	(a)				(a)	(a)				(a)	(a)				(a)	(a)	
30	1	6.318	0.323	0.239	1	3	3.141 3.265 3.519	0.231 0.242 0.266	0.105			5.483 6.308 7.061	0.427 0.223 0.234	0.205 0.114 0.126					
80	4	3.285 3.590 5.301 6.392	0.298 0.313 0.428 0.272	0.204 0.225 0.206 0.170	0					1180	4	3.256 5.211 5.557 6.953	0.418 0.343 0.349 0.202	0.200 0.162 0.165 0.094	1	2	3.601 3.759	0.273 0.409	0.131
120	4	3.204 4.351 5.008 5.468	0.125 0.423 0.453 0.467	0.036 0.203 0.216 0.225	0					1223	6	3.263 3.835 5.700 6.097	0.165 0.396 0.311 0.279	0.062 0.189 0.222 0.179	0				
160	2	3.270 7.024	0.248 0.273	0.141 0.171	0					1261	2	6.419 7.061 3.274	0.188 0.217 0.105	0.081 0.108 0.025	0				
195	4	4.363 5.685 7.024	0.261 0.518 0.240	0.156 0.251 0.132	0					1311	3	7.062 4.259 6.002	0.226 0.844 0.228	0.117 0.414 0.119	1	2	3.158 3.399	0.210 0.273	0.068
240	1	7.019	0.236	0.128	0					1359	3	6.949 4.158 5.969 6.950	0.277 0.769 0.398 0.224	0.176 0.376 0.190 0.115	2	3	3.207 3.325 3.674 4.999 4.915 5.501	0.271 0.323 0.375 0.695 0.329 0.309	0.461
270	3	3.235 5.669 7.036	0.186 0.271 0.230	0.079 0.168 0.121	0														
325	3	3.283 6.313 7.027	0.327 0.166 0.247	0.245 0.063 0.140	0														
365	2	6.371 6.933	0.374 0.091	0.178 0.019	1	3	3.159 3.341 3.546	0.283 0.202 0.276	0.113	1411	2	3.313 7.054 3.602	0.130 0.300 0.239	0.039 0.206 0.131	0				
400	3	3.272 3.780 7.036	0.277 0.488 0.116	0.176 0.236 0.031	0					1441	5	4.387 6.085 6.435	0.312 0.285 0.117	0.223 0.186 0.031	0				
443	2	3.270 3.819	0.251 0.104	0.145 0.025	0							7.069 3.347 3.626	0.107 0.366 0.193	0.026 0.174 0.085	0				
489	3	3.282 5.395 7.030	0.224 0.507 0.168	0.115 0.245 0.065	0					1486	3	4.512 3.206 3.719	0.646 0.197 0.137	0.315 0.089 0.043	1	3	6.008 6.175 6.375	0.316 0.260 0.303	0.149
519	4	3.278 5.395 6.295	0.263 0.325 0.264	0.159 0.242 0.160	0					1521	3	6.958 3.304 3.570	0.269 0.210 0.172	0.166 0.101 0.068	0				
564	3	7.026 3.289	0.126 0.277	0.036 0.176	0					1600	5	4.380	0.316	0.229					

		3.787	0.223	0.114						6.122	0.230	0.121							
		7.042	0.249	0.142						7.065	0.254	0.148							
601	3	3.324	0.272	0.170	0				1640	3	3.629	0.147	0.050	0					
		3.774	0.229	0.120							6.398	0.184	0.078						
		7.048	0.243	0.130							7.060	0.129	0.038						
653	2	3.305	0.163	0.061	0				1690	3	3.523	0.162	0.060	1	4	5.563	0.333	0.176	
		3.787	0.422	0.202							4.466	0.314	0.220			5.830	0.200		
685	2	3.301	0.286	0.188	0						6.963	0.144	0.048			6.077	0.294		
		3.804	0.433	0.208												6.302	0.265		
715	5	3.348	0.258	0.153	0				1733	4	3.321	0.190	0.083	0					
		3.608	0.258	0.153							3.825	0.260	0.155						
		5.439	0.399	0.189							4.478	0.474	0.229						
		6.320	0.386	0.184							7.068	0.162	0.060						
		7.065	0.282	0.182							3.317	0.223	0.114	0					
754	4	3.610	0.085	0.017	0				1766	2	6.440	0.160	0.059						
		5.592	0.270	0.167					1813	1	3.241	0.153	0.054	2	2	3.466	0.239	0.226	
		6.257	0.504	0.244												3.757	0.343		
		7.022	0.221	0.112												5.983	0.363		
799	3	3.821	0.322	0.238	0											6.316	0.302		
		6.263	0.391	0.187					1858	2	3.333	0.131	0.039	0					
		7.043	0.140	0.045							6.308	0.163	0.061						
833	2	3.219	0.135	0.042	0				1890	4	3.235	0.181	0.075	1	2	3.541	0.244	0.046	
		6.119	0.443	0.213							6.018	0.364	0.173			3.712	0.143		
883	3	3.230	0.157	0.057	0						6.375	0.246	0.139						
		5.518	0.376	0.179							6.982	0.172	0.068						
		7.048	0.247	0.140					1927	5	3.284	0.220	0.111	0					
927	5	3.342	0.332	0.253	0						3.560	0.203	0.095						
		3.849	0.384	0.183							4.360	0.270	0.167						
		5.522	0.273	0.171							4.588	0.186	0.079						
		6.105	0.225	0.116							7.058	0.221	0.112						
		7.060	0.259	0.154					1965	3	3.297	0.162	0.060	0					
958	3	3.363	0.225	0.116	0						3.830	0.177	0.072						
		6.106	0.210	0.101							7.072	0.143	0.047						
		7.068	0.155	0.055					2000	2	3.294	0.166	0.063	0					
1001	1	6.025	0.165	0.062	1	2	3.223	0.319	0.195		4.388	0.207	0.098						
							3.677	0.589		2029	4	3.320	0.181	0.075	0				
1063	5	3.286	0.244	0.137	0						3.839	0.318	0.232						
		3.615	0.259	0.154							6.111	0.319	0.233						
		6.127	0.328	0.247							7.083	0.243	0.135						
		6.349	0.117	0.031					2069	5	3.324	0.290	0.193	0					
		7.059	0.314	0.226							3.631	0.324	0.241						
1095	4	3.295	0.248	0.141	0						4.367	0.277	0.176						
		3.817	0.332	0.253							6.296	0.130	0.039						
		6.325	0.416	0.199							7.075	0.250	0.143						
		7.063	0.326	0.244					2117	4	3.314	0.176	0.071	0					
1140	4	3.274	0.221	0.112	0						3.779	0.288	0.190						

^a4.054 movie analyzer units equal 0.75 inch; left end reading, 3.136; right end reading, 7.190.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(f) Concluded. Test fluid, methanol; run 63-1-14-6

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area frac-tion, φ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, φ_m		Sites	Bubble center	Bubble width	Area frac-tion, φ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, φ_m
	(a)	(a)	(a)			(a)	(a)		(a)		(a)	(a)	(a)		(a)	(a)		(a)	
2152	4	4.564	0.224	0.115	0					3025	0	3.615	0.212	0.103	1	2	3.191	0.220	0.053
		7.060	0.203	0.095								6.479	0.231	0.122					
		3.264	0.211	0.102								7.043	0.219	0.110					
		6.109	0.418	0.200															
		6.393	0.150	0.052															
2192	1	7.050	0.187	0.080	0					3063	5	3.310	0.153	0.054	0				
		3.248	0.121	0.034								3.813	0.325	0.242					
		3.329	0.138	0.044								4.366	0.112	0.029					
		4.568	0.212	0.103								5.867	0.372	0.177					
		6.091	0.366	0.174								6.465	0.273	0.171					
2237	3	3.332	0.180	0.074	0					3103	4	3.323	0.182	0.076	0				
		3.775	0.248	0.141								4.518	0.431	0.207					
		4.359	0.413	0.198								5.098	0.466	0.225					
		6.293	0.315	0.228								7.028	0.235	0.127					
		7.065	0.279	0.179								3.334	0.218	0.109					
2317	5	3.321	0.326	0.244	0					3146	7	3.566	0.246	0.139	0				
		3.809	0.359	0.170								3.873	0.369	0.175					
		5.164	0.480	0.232								4.601	0.324	0.241					
		5.849	0.395	0.189								5.133	0.178	0.073					
		7.085	0.265	0.161								6.487	0.253	0.147					
2347	6	3.313	0.173	0.069	0					3193	4	7.038	0.254	0.148	0				
		4.375	0.111	0.028								3.291	0.280	0.180					
		4.593	0.324	0.241								3.536	0.210	0.101					
		5.129	0.648	0.316								4.363	0.419	0.201					
		5.817	0.592	0.288								6.070	0.189	0.082					
2397	4	7.065	0.172	0.068	0					3228	4	3.256	0.193	0.085	0				
		3.400	0.268	0.165								4.382	0.123	0.035					
		3.804	0.332	0.253								5.869	0.296	0.201					
		6.058	0.218	0.109								6.490	0.208	0.099					
		6.383	0.234	0.126								3.246	0.090	0.019					
2437	4	3.268	0.202	0.094	0					3273	2	6.103	0.264	0.160	0				
		4.346	0.317	0.231								3.203	0.179	0.073					
		5.138	0.276	0.175								6.510	1.059	0.520					
		6.405	0.280	0.180								3.157	0.195	0.087					
		3.322	0.244	0.137								3.403	0.297	0.202					
2473	5	3.825	0.403	0.193	0					3359	4	4.457	0.224	0.115	2	2	3.749	0.260	0.213
		6.086	0.318	0.232								6.942	0.249	0.142					
		6.416	0.129	0.038								3.312	0.430	0.207					
		7.038	0.265	0.161								5.901	0.383	0.183					
		3.268	0.185	0.079								6.306	0.426	0.205					

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(g) Test fluid, methanol; run 63-2-6-1

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles						
	Sites	Bubble center	Bubble width	Area frac-tion, φ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, φ_m		Sites	Bubble center	Bubble width	Area frac-tion, φ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, φ_m		
	(a)	(a)			(a)	(a)					(a)	(a)			(a)	(a)					
0	3	5.228	0.487	0.261	2	2	2.756	0.219	0.209	1033	3	3.549	0.497	0.267	0						
		5.807	0.209	0.122			2.898	0.121				4.658	0.540	0.291							
		6.264	0.136	0.052			3.548	0.406				6.105	0.393	0.209							
30	3	3.538	0.365	0.193	1	2	3.904	0.307	0.023	1063	3	2.727	0.202	0.114	0						
		5.228	0.203	0.116			2.708	0.134				4.880	0.344	0.181							
		6.156	0.299	0.251			2.809	0.104				6.065	0.350	0.185							
80	5	2.738	0.223	0.139	1	2	5.720	0.520	0.195	1095	1	2.767	0.252	0.178	0						
		3.561	0.467	0.250			6.128	0.297				4.700	0.210	0.124							
		4.694	0.293	0.241								6.101	0.286	0.229							
120	2	5.232	0.286	0.229	2	2	2.774	0.255	0.342	1140	5	4.018	0.575	0.310	1	3	2.761	0.219	0.188		
		6.288	0.075	0.016													2.911	0.327			
		3.527	0.535	0.288			2.774	0.255				0.342	1140	5			2.768	0.200	0.112	0	
160	2	6.111	0.402	0.214	2	2	3.056	0.428	0.248	1180	2	3.877	0.309	0.161	2	2	3.303	0.545	0.404		
							4.494	0.479				4.697	0.788	0.427			3.691	0.320			
							4.828	0.317				5.665	0.677	0.366			5.808	0.233			
195	3	5.260	0.461	0.247	1	3	2.728	0.314	0.055	1223	2	6.201	0.246	0.170	2	2	6.093	0.390	0.275		
		6.223	0.219	0.134			2.955	0.141				2.804	0.273	0.209			2	2		6.166	0.294
							3.342	0.632				4.187	0.773	0.419						2.701	0.107
240	5	3.272	0.220	0.136	1	2	2.674	0.247	0.055	1261	2	4.214	0.549	0.296	2	2	2.795	0.137	0.206		
		5.276	0.248	0.172													5.716	0.718			
		6.216	0.195	0.107													6.150	0.303			
325	4	2.767	0.227	0.144	0					1311	3	2.770	0.206	0.119	1	4	5.719	0.299	0.103		
		3.560	0.201	0.113													5.862	0.316			
		5.261	0.408	0.217													5.918	0.225			
365	2	6.141	0.366	0.194	0					1359	1	3.590	0.353	0.186	2	2	6.107	0.235	0.268		
		2.738	0.175	0.086													5.779	0.311			
		6.110	0.407	0.217													5.889	0.224			
400	3	2.779	0.264	0.195	0					1411	2	2.739	0.194	0.106	1	3	3.235	0.383	0.351		
		4.675	0.279	0.218													6.223	0.163			
		6.144	0.307	0.160													0.074	0.074			
443	4	2.763	0.229	0.147	0					1441	0	4.629	0.371	0.196	1	3	2.741	0.143	0.241		
		3.541	0.504	0.271													6.149	0.313			
		5.200	0.196	0.108														0.057			
489	4	6.265	0.097	0.026	0										1	3	4.056	0.457	0.241		
		2.754	0.215	0.130													2.717	0.095			
																	2.818	0.258			

Total number of sample frames, k , 50.
Total number of single bubbles, h , 139.
Total number of merging bubbles, 86.
Average instantaneous bubble population, n_{av} , 4.50.
Average area fraction of influence of single bubble, $\phi_{s,av}$, 0.186.
Average area fraction of merging bubbles, $\phi_{m,av}$, 0.1147.
Standard deviation associated with $\phi_{m,av}$, 0.1350.

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TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(h) Test fluid, methanol; run 63-2-6-2

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m		Sites	Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m
	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)		(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)
30	3	3.072 4.094 6.510	0.378 0.354 0.313	0.195 0.182 0.159	2	3	4.697 4.884 4.983	0.637 0.273 0.315	0.640	601	4	3.033 4.066 5.012 6.431	0.387 0.449 0.101 0.393	0.200 0.234 0.027 0.204	0	2	3.452 3.949 4.104	0.470 0.238 0.290	
80	5	3.224 4.252 4.674 5.050 6.429	0.480 0.518 0.328 0.176 0.325	0.251 0.272 0.166 0.083 0.166	1	3	5.400 5.585 5.766 5.900	0.402 0.271 0.298 0.481	0.227	653	4	3.055 5.008 5.635 6.472	0.434 0.103 0.342 0.351	0.226 0.028 0.176 0.181	0				
120	4	3.083 4.144 5.652 6.444	0.326 0.417 0.286 0.327	0.167 0.217 0.219 0.167	0					685	4	3.016 3.907 5.000 6.398	0.304 0.492 0.251 0.540	0.247 0.258 0.168 0.284	0				
160	1	6.445	0.401	0.208	2	3	3.118 3.460 4.053 4.692 4.959 5.292 5.676	0.367 0.929 0.392 0.365 0.218 0.475 0.335	0.724	715	4	3.028 3.833 5.051 6.551	0.347 0.292 0.732 0.200	0.178 0.228 0.387 0.107	0				
195	6	3.045 3.601 3.928 5.176 5.621 6.452	0.391 0.163 0.355 0.429 0.358 0.415	0.203 0.071 0.183 0.223 0.184 0.216	0					754	2	3.090 6.350	0.370 0.367	0.191 0.189	1	4	4.853 4.908 5.183 5.217	0.211 0.292 0.278 0.240	0.177
240	2	5.032 6.484	0.170 0.358	0.077 0.184	2	2	3.076 3.120 3.544 3.878	0.282 0.371 0.321 0.460	0.341	799	3	3.044 4.994 6.376	0.441 0.130 0.481	0.230 0.045 0.252	0				
						3				833	3	3.034 4.987 6.462	0.361 0.093 0.301	0.186 0.023 0.242	0				
										883	1	6.392	0.383	0.198	1	5	3.054 3.625	0.343 0.798	0.737

270	2	5.014 6.434	0.175 0.322	0.082 0.164	1	4	4.132 3.213 3.573 3.780 3.978 3.119 3.128 3.483	0.179 0.505 0.339 0.319 0.418 0.363 0.416 0.305	0.368									4.347 4.919 5.258 3.149 3.218 3.656 3.728 3.948 4.068 3.076 3.503 3.722 6.203 6.495	0.646 0.555 0.588 0.390 0.330 0.259 0.403 0.371 0.209 0.415 0.438 0.197 0.280 0.304				
325	3	3.995 4.759 6.502	0.402 0.286 0.318	0.209 0.219 0.162	1	3	3.119 3.128 3.483	0.363 0.416 0.305	0.244		927	3	4.932 5.185 6.375	0.183 0.194 0.453	0.090 0.101 0.236	2	2	4	3.149 3.218 3.656 3.728 3.948 4.068 3.076 3.503 3.722 6.203 6.495	0.390 0.330 0.259 0.403 0.371 0.209 0.415 0.438 0.197 0.280 0.304	0.418		
365	5	3.107 4.674 4.726 6.130 6.514 6.407	0.295 0.290 0.172 0.252 0.318 0.424	0.233 0.225 0.079 0.170 0.162 0.221	0						958	2	5.000 5.320	0.111 0.403	0.033 0.209	2	3	2	3.076 3.503 3.722 6.203 6.495	0.415 0.438 0.197 0.280 0.304	0.345		
400	1				2	3	3.092 3.100 3.439 4.451 4.968 5.077 3.029 3.277 4.889 5.129	0.282 0.260 0.474 0.485 0.549 0.306 0.269 0.219 0.397 0.355	0.535		1001	3	3.054 5.317 6.471 6.363	0.281 0.521 0.315 0.471	0.211 0.273 0.161 0.246	0		2	3.010 3.491 5.032 5.313 3.464 3.562 3.829 4.137 3.045 3.264 3.774 4.905 5.069 3.850 4.196 5.476 5.558 5.841	0.386 0.577 0.419 0.264 0.241 0.223 0.263 0.698 0.251 0.186 0.882 0.217 0.141 0.311 0.380 0.292 0.357 0.439	0.382		
443	2	5.592 6.424	0.429 0.316	0.223 0.161	2	2	3.277 4.889 5.129	0.219 0.397 0.355	0.254		1063	2	3.066 6.461	0.271 0.386	0.196 0.200	2	2	2	3.464 3.562 3.829 4.137 3.045 3.264 3.774 4.905 5.069 3.850 4.196 5.476 5.558 5.841	0.241 0.223 0.263 0.698 0.251 0.186 0.882 0.217 0.141 0.311 0.380 0.292 0.357 0.439	0.298		
489	5	3.052 3.524 4.442 5.010 6.408	0.377 0.776 0.653 0.123 0.477	0.195 0.410 0.344 0.040 0.249	0						1095	2	5.694 6.512	0.781 0.201	0.413 0.108	2	3	2	3.045 3.264 3.774 4.905 5.069 3.850 4.196 5.476 5.558 5.841	0.251 0.186 0.882 0.217 0.141 0.311 0.380 0.292 0.357 0.439	0.340		
519	2	5.632 6.391	0.305 0.419	0.249 0.218	1	5	3.150 3.667 4.025 4.501 4.948 3.050 3.333 3.045	0.500 0.534 0.618 0.335 0.559 0.333 0.230	0.629		1140	3	3.107 4.978 6.421	0.254 0.091 0.328	0.172 0.022 0.168	2	2	3	3.850 4.196 5.476 5.558 5.841	0.311 0.380 0.292 0.357 0.439	0.397		
564	2	4.944 6.476	0.178 0.335	0.085 0.172	2	3	3.050 3.045	0.333 0.230	0.317														

Total number of sample frames, k , 56.
 Total number of single bubbles, h , 155.
 Total number of merging bubbles, 187.
 Average instantaneous bubble population, n_{av} , 6.11.
 Average area fraction of influence of single bubble, $\varphi_{s,av}$, 0.185.
 Average area fraction of merging bubbles, $\varphi_{m,av}$, 0.2548.
 Standard deviation associated with $\varphi_{m,av}$, 0.2254.

^a3.755 movie analyzer units equal 0.75 inch; left end reading, 2.895; right end reading, 6.650.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER.

[1/16- by 3/4-in. heating strip.]

(1) Test fluid, methanol; run 63-2-6-3

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area fraction, Φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, Φ_m		Sites	Bubble center	Bubble width	Area fraction, Φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, Φ_m
		(a)	(a)				(a)	(a)					(a)	(a)			(a)	(a)	
0	1	5.008	0.153	0.063	1	5	3.038 3.263 3.535 3.986 4.375	0.229 0.220 0.550 0.353 0.465	0.401	1001	3	3.026 3.376 4.394	0.315 0.431 0.432	0.161 0.226 0.226	1	5	3.942 3.026 3.135 3.339 3.566 3.858	0.351 0.205 0.734 0.209 0.225 0.378	0.361
30	3	3.081 3.549 6.335	0.435 0.367 0.538	0.220 0.190 0.284	1	4	4.117 4.501 4.905 5.514	0.446 0.322 0.459 0.758	0.485	1033	2	3.076 4.341	0.302 0.230	0.246 0.143	2	2	4.470 3.172 3.953	0.202 0.429 0.372	0.361
80	2	3.681 6.391	0.313 0.438	0.160 0.229	1	4	3.840 4.435 4.900 5.032	0.791 0.399 0.531 0.233	0.471	1095	3	3.017 4.402 4.968	0.291 0.612 0.256	0.224 0.324 0.180	0	2	3.327 3.953 0.566	0.566	
120	6	3.066 3.670 4.232 4.745 5.311 6.434	0.273 0.365 0.315 0.297 0.313 0.398	0.201 0.189 0.161 0.238 0.160 0.207	0					1140	1	6.470	0.232	0.215	1	7	3.036 3.219 3.729 4.061 4.489 4.860 5.292	0.250 0.617 0.403 0.549 0.348 0.415 0.312	0.791
160	3	3.082 3.871 6.455	0.315 0.666 0.321	0.161 0.355 0.165	1	3	4.363 4.612 4.867	0.326 0.464 0.190	0.207	1180	1	6.333	0.433	0.227	2	4	3.083 3.722 4.401 4.441 4.777 5.052	0.241 0.490 0.409 0.262 0.247 0.302	0.717
195	2	3.083 3.858	0.380 0.334	0.193 0.172	2	4	4.331 4.647 5.038 5.376 5.910 6.325	0.211 0.421 0.361 0.347 0.472 0.370	0.355	1223	1	4.367	0.290	0.227	2	3	3.695 3.311 3.550 3.580 4.096 6.190	0.374 0.237 0.341 0.306 0.352 0.306	0.407
240	6	3.092 3.841 4.412 4.794 5.119 6.510	0.341 0.796 0.192 0.235 0.131 0.302	0.176 0.423 0.100 0.149 0.046 0.246	1	2	5.492 5.809	0.338 0.297	0.133	1261	3	3.066 4.730 4.987	0.315 0.285 0.237	0.161 0.219 0.152	1	3	3.522 3.769 4.074	0.324 0.290 0.430	0.224
270	5	3.110 3.715 4.416 5.745 6.424	0.281 0.293 0.371 0.413 0.474	0.213 0.232 0.193 0.210 0.244	1	2	4.896 5.224	0.322 0.401	0.163	1311	5	4.424 4.794 4.785 5.601 6.164	0.209 0.135 0.162 0.452 0.243	0.113 0.097 0.071 0.237 0.237	1	3	3.002 3.015 3.346 3.693 4.381	0.254 0.273 0.355 0.333 0.242	0.367
325	2	3.097 3.690	0.342 0.343	0.176 0.177	2	2	2.987 3.198 3.447 5.087 5.367 6.215 6.477	0.273 0.266 0.556 0.336 0.342 0.346 0.179	0.483	1350	2	3.677 6.451	0.250 0.167	0.250 0.075	2	2	3.114 3.308 4.133 4.224 4.302	0.340 0.371 0.444 0.301 0.311	0.403
365	2	3.097 3.690	0.342 0.343	0.176 0.177	2	2	3.833 4.372 6.132 6.543	0.427 0.640 0.496 0.337	0.463	1411	1	3.649	0.284	0.211	2	2	2.794 3.223 3.594 3.715	0.201 0.333 0.364 0.375	0.333
400	1	3.026	0.369	0.253	1	6	4.054 4.463 4.712 5.502 5.746 6.401	0.250 0.568 0.855 0.365 0.366 0.460	0.691	1461	3	2.991	0.252	0.133	2	3	4.717	0.717	0.553
443	2	4.421 6.413	0.254 0.307	0.174 0.264	2	2	4.031 5.143	0.285 0.240	0.26	1461	3	2.991	0.252	0.133	2	3	4.717	0.717	0.553

						2	4.933	0.300			3.524	0.283	0.210		4.993	0.333		
							5.314	0.463			4.087	0.441	0.231		5.000	0.386		
489	3	3.034	0.363	0.185	2	2	4.927	0.715	0.347					2	5.061	0.793		
		3.718	0.684	0.363			5.286	0.502							5.420	0.341		
		4.397	0.242	0.158		2	5.231	0.363		1486	3	3.001	0.298	0.240	2	4.115	0.349	0.290
							6.457	0.441				4.873	0.411	0.215		4.432	0.285	
519	1	6.516	0.181	0.083	1	9	3.155	0.509	0.733			6.431	0.389	0.202	2	5.879	0.331	
							3.494	0.168							5.948	0.355		
							3.651	0.147		1521	5	3.674	0.383	0.199	0			
							3.569	0.274				3.584	0.202	0.110				
							3.967	0.546				4.133	0.199	0.107				
							4.448	0.416				4.495	0.345	0.178				
							4.812	0.313				6.388	0.477	0.251				
							5.004	0.322		1571	4	3.061	0.395	0.206	1	4.017	0.365	0.150
							3.302	0.385				3.496	0.383	0.199		4.367	0.335	
564	4	4.028	0.403	0.210	1	3	3.075	0.365	0.168			5.860	0.515	0.271				
		4.771	0.322	0.165			3.344	0.172				6.435	0.387	0.201				
		5.309	0.301	0.245			3.584	0.308		1600	1	5.023	0.695	0.367	2	5		
		6.453	0.501	0.264														
601	2	3.175	0.633	0.335	1	4	3.975	0.271	0.483						5.129	0.421	3.714	
		6.561	0.284	0.218			4.334	0.533							3.461	0.365		
							4.850	0.550							5.024	0.479		
							5.272	0.626							4.058	0.389		
653	3	4.389	0.506	0.266	1	2	3.065	0.331	0.141					3	4.390	0.274		
		5.365	0.677	0.359			3.296	0.319							5.799	0.452		
		6.233	0.748	0.397											6.179	0.307		
685	1	4.477	0.212	0.121	2	2	3.063	0.338	0.492	1640	2	5.967	0.451	0.236	3	5.072	0.311	0.543
							3.405	0.517				6.409	0.350	0.181		5.386	0.429	
						4	5.660	0.245							3	3.744	0.257	
							5.955	0.345								4.003	0.261	
							5.911	0.330							2	4.376	0.484	
							6.326	0.409								4.895	0.260	
715	2	3.031	0.290	0.227	2	2	3.829	0.356	0.422	1690	3	3.037	0.322	0.165	1	5.248	0.478	
		5.484	0.576	0.364			4.353	0.693				3.969	0.506	0.266	2	4.916	0.248	0.154
						2	4.911	0.373				6.318	0.555	0.293		5.270	0.460	
							4.960	0.340				3.076	0.407	0.212	2	5.122	0.272	0.389
754	2	3.075	0.361	0.187	2	3	4.371	0.635	0.420	1733	3	3.961	0.167	0.075	2	5.329	0.520	
		6.399	0.375	0.195			4.883	0.388				4.381	0.145	0.057	2	5.806	0.529	
							5.024	0.287								6.338	0.535	
						2	5.439	0.212		1766	4	3.056	0.373	0.194	0			
							5.447	0.354				3.910	0.173	0.081				
799	3	3.096	0.347	0.177	1	2	6.057	0.329	0.165			4.997	0.144	0.052				
		3.930	0.455	0.239			6.418	0.393				6.378	0.499	0.263				
		4.914	0.261	0.184						1813	4	2.980	0.182	0.089	1	3.070	0.569	0.199
833	3	3.060	0.287	0.222	1	2	3.661	0.816	0.274			4.387	0.294	0.233	2	3.878	0.284	
		4.355	0.382	0.199			3.401	0.302				5.761	0.612	0.324				
		6.368	0.489	0.257								6.380	0.469	0.246				
863	2	3.069	0.295	0.235	3	3	3.631	0.265	0.619	1858	3	3.054	0.289	0.225	2	3.079	0.315	0.447
		4.354	0.307	0.254			3.895	0.311				5.023	0.333	0.171		4.029	0.384	
							3.938	0.409				6.384	0.477	0.251	2	5.468	0.620	
						3	4.866	0.179								5.810	0.523	
							5.039	0.167		1890	2	4.964	0.256	0.177	2	3.137	0.427	0.601
							5.484	0.842				5.536	0.600	0.317		3.393	0.315	
						2	6.106	0.178								3.646	0.378	
							6.448	0.506								3.818	0.244	
958	1	6.624	0.185	0.092	2	7	3.081	0.302	0.677							4.028	0.386	
							3.400	0.337								4.406	0.371	
							3.677	0.217								6.278	0.298	
							3.875	0.178								6.458	0.313	
							4.003	0.295		1927	4	3.072	0.247	0.165	1	6.110	0.190	0.127
							4.206	0.294				4.406	0.650	0.345		6.418	0.427	
							4.379	0.275				4.896	0.237	0.152				
						3	5.125	0.718				5.476	0.488	0.257				
							5.625	0.283										

^a3.737 movie analyzer units equal 0.75 inch; left end reading, 2.886; right end reading, 6.623.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(1) Concluded. Test fluid, methanol; run 63-2-6-3

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area frac- tion, Φ_s	Sites	Number of merg- ing bub- bles	Site center	Site width	Area frac- tion, Φ_m		Sites	Bubble center	Bubble width	Area frac- tion, Φ_s	Sites	Number of merg- ing bub- bles	Site center	Site width	Area frac- tion, Φ_m
(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	
1180	2	4.166 4.970	0.350 0.095	0.180 0.024	2	2	3.050 3.128	0.268 0.273	0.394	1813	4	6.044 4.326 4.925 5.566 6.396	0.303 0.860 0.124 0.332 0.298	0.245 0.456 0.041 0.170 0.237	1	2	2.950 2.985	0.195 0.199	0.052
1223	2	3.045 5.454	0.160 0.325	0.068 0.166	3	3	3.449 3.858 4.205 4.943 4.855 5.841 6.180	0.499 0.318 0.377 0.654 0.231 0.339 0.433	0.660	1858	2	5.569 6.502	0.333 0.216	0.171 0.125	3	2	3.001 3.083 4.165 4.306 4.310 4.563 4.846	0.197 0.262 0.176 0.157 0.172 0.334 0.206	0.257
1261	2	3.067 4.994	0.356 0.371	0.183 0.192	1	2	3.743 4.063	0.293 0.346	0.135								4.819 4.953	0.089 0.179	
1311	4	3.029 4.223 4.856 6.396 4.894	0.359 0.571 0.278 0.407 0.138	0.185 0.300 0.207 0.211 0.051	0					1890	2	2.918 5.203	0.288 0.611	0.222 0.322	2	5	4.189 4.360 4.324 4.618 4.763 6.039 6.360	0.337 0.230 0.256 0.351 0.191 0.324 0.318	0.394
1359	1				3	3	3.044 3.053 3.477	0.357 0.368 0.585	0.803								6.360 2.954 3.038 4.135 4.401 4.637 4.903	0.318 0.243 0.211 0.281 0.250 0.358 0.304	0.307
						2	4.389 4.617	0.396 0.359		1927	3	5.231 5.597 6.519	0.189 0.319 0.351	0.096 0.163 0.181	2	2	2.954 3.038 4.135 4.401 4.637 4.903	0.243 0.211 0.281 0.250 0.358 0.304	
1411	0				2	4	3.000 3.105 3.202 3.483 5.828	0.247 0.341 0.286 0.373 0.376	0.466	1965	2	3.022 6.526	0.315 0.226	0.161 0.137	1	3	4.736 5.198 5.608	0.407 0.517 0.302	0.286

1441	0				3	2	6.263	0.495	0.598	2000	2	4.597	0.097	0.025	3	6	3.064	0.155	0.355
							2.981	0.183				5.583	0.094	0.024			3.036	0.120	
						3	3.051	0.263									2.952	0.168	
							4.843	0.675									3.110	0.149	
							4.809	0.270									3.036	0.224	
							5.214	0.541									3.232	0.169	
						2	5.987	0.357								2	5.144	0.330	
							6.360	0.389									5.281	0.193	
1486	4	3.033	0.367	0.189	1	4	4.746	0.236	0.199							2	6.023	0.303	
		5.725	0.334	0.171			4.791	0.250									6.360	0.371	
		6.006	0.272	0.198			5.009	0.290		2029	2	3.061	0.392	0.203	1	2	4.575	0.497	0.225
		6.376	0.406	0.211			5.290	0.310				6.371	0.385	0.199			4.887	0.424	
1521	2	2.997	0.308	0.254	2	3	4.301	0.542	0.456	2069	3	3.155	0.292	0.228	1	2	4.938	0.106	0.022
		6.057	0.311	0.259			4.691	0.238				5.579	0.309	0.255			4.943	0.147	
							4.709	0.275				6.402	0.365	0.188					
						3	5.211	0.396		2117	5	3.019	0.375	0.194	0				
							5.622	0.427				4.574	0.493	0.258					
							5.881	0.233				4.919	0.141	0.053					
1571	3	3.064	0.267	0.191	1	2	5.417	0.270	0.138			5.557	0.338	0.173					
		4.841	0.393	0.204			5.744	0.384				6.503	0.265	0.188					
		6.295	0.487	0.255						2152	3	3.032	0.291	0.226	1	2	4.601	0.294	0.142
1600	3	3.053	0.440	0.229	0							5.564	0.195	0.102			4.931	0.366	
		6.196	0.258	0.178								6.433	0.362	0.187					
		6.423	0.331	0.169						2192	3	2.995	0.262	0.184	0				
1640	2	3.068	0.402	0.209	1	4	4.847	0.246	0.350			5.195	0.670	0.354					
		6.292	0.571	0.300			4.855	0.515				6.443	0.271	0.196					
							5.198	0.372		2237	6	2.969	0.275	0.202	1	2	5.959	0.389	0.187
							5.585	0.403				4.873	0.205	0.112			6.269	0.405	
1690	2	5.083	0.155	0.064	2	2	2.985	0.227	0.252			4.962	0.161	0.069					
		5.561	0.237	0.150		2	3.186	0.250				5.161	0.165	0.073					
							5.945	0.419				5.353	0.240	0.154					
							6.291	0.341				5.586	0.298	0.237					
1733	5	2.968	0.267	0.191	0					2274	2	2.961	0.259	0.179	1	3	4.715	0.340	0.218
		4.835	0.302	0.244								6.378	0.514	0.269			4.900	0.120	
		5.164	0.392	0.203													5.210	0.531	
		5.598	0.243	0.158															

Total number of sample frames, k , 47.
 Total number of single bubbles, h , 130.
 Total number of merging bubbles, 202.
 Average instantaneous bubble population, n_{av} , 7.06.
 Average area fraction of influence of single bubble, $\phi_{s,av}$, 0.208.
 Average area fraction of merging bubbles, $\phi_{m,av}$, 0.5695.
 Standard deviation associated with $\phi_{m,av}$, 0.2142.

^a3.737 movie analyzer units equal 0.75 inch; left end reading, 2.886; right end reading, 6.623.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(j) Test fluid, methanol; run 63-2-6-4

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area frac-tion, ϕ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, ϕ_m		Sites	Bubble center	Bubble width	Area frac-tion, ϕ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, ϕ_m
		(a)	(a)				(a)	(a)					(a)	(a)				(a)	(a)
30	4	4.664 4.811 5.320 6.227	0.156 0.165 0.263 0.427	0.060 0.074 0.197 0.224	1	5	2.852 3.138 3.645 4.020 4.364 4.420	0.391 0.431 0.582 0.268 0.420	0.497						4	5.391 5.724 5.851 6.229	0.341 0.548 0.373 0.462		
80	1	6.243	0.321	0.166	3	3	2.915 3.285 3.630 4.834 4.704 5.440	0.354 0.387 0.303 0.276 0.535 0.451	0.616	489	2	4.821 6.191	0.191 0.481	0.099 0.254	1	7	2.854 3.126 3.354 3.595 3.854 4.289 3.929	0.309 0.234 0.313 0.169 0.361 0.582 0.399	0.516
120	1	4.848	0.471	0.249	2	5	2.913 3.267 3.576 3.631 4.050 5.821 6.305	0.419 0.350 0.273 0.320 0.518 0.502 0.467	0.673	519	2	4.335 4.792	0.396 0.221	0.207 0.133	2	4	2.884 3.175 3.499 3.797 5.813 6.239	0.298 0.284 0.365 0.466 0.424 0.429	0.522
160	3	4.149 5.865 6.247	0.270 0.299 0.363	0.199 0.244 0.189	2	6	2.858 2.983 3.098 3.158 3.360 3.702 4.592 4.909 5.102 5.284	0.201 0.109 0.131 0.132 0.272 0.412 0.244 0.391 0.194 0.514	0.497	564	1	6.170	0.574	0.305	1	6	3.097 3.471 3.858 4.435 4.785 2.881 3.136 3.371 4.496 4.577 4.893 5.584	0.361 0.387 0.386 0.768 0.426 0.280 0.230 0.240 0.300 0.307 0.510 0.644	0.633
195	3	2.875 3.688 4.373	0.315 0.553 0.303	0.162 0.183 0.250	2	2	4.986 5.346 5.705 6.214	0.323 0.433 0.376 0.399	0.357	601	0				3	3	3.165 3.264 4.718 5.135 5.250 5.569 5.745 6.138 2.898 3.220 3.786 4.390 4.464	0.310 0.280 0.461 0.659 0.267 0.259 0.216 0.635 0.337 0.306 0.926 0.247 0.255	0.705
240	2	5.377 6.283	0.317 0.341	0.163 0.177	1	8	2.893 3.144 3.448 3.708 4.069 4.363 4.831 4.775 2.874 2.777 2.999 3.252	0.374 0.351 0.333 0.587 0.310 0.446 0.491 0.269 0.171 0.129 0.236 0.211	0.736	653	2	3.543 4.139	0.160 0.191	0.070 0.099	2	3			
270	1	6.191	0.610	0.324	2	12			0.567	685	1	6.391	0.278	0.211	1	10			0.672

^a3.720 movie analyzer units equal 0.75 inch; left end reading, 2.743, right end reading, 6.463.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(j) Concluded. Test fluid, methanol; run 63-2-6-4

(J) Continued. rest fluid, methanol; run 63-2-6-4

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m		Sites	Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m
						2	3.562	0.275		1600	2	5.021	0.121	0.040	1	4	2.880	0.725	0.263
						1	4.078	0.131				6.352	0.216	0.127			2.912	0.298	
							4.810	0.249									3.110	0.235	
							4.955	0.235									3.482	0.508	
							5.036	0.309		1640	1	2.912	0.365	0.190	3	2	3.322	0.340	0.801
							5.315	0.249									3.555	0.201	
							5.513	0.147								3	4.276	0.596	
							5.776	0.378									4.750	0.352	
							6.205	0.480									4.837	0.475	
1001	3	2.832	0.308	0.250	2	3	3.383	0.521	0.546							3	5.452	0.417	
		4.810	0.341	0.177			3.723	0.453									5.885	0.448	
		5.234	0.326	0.160			4.103	0.468									6.138	0.537	
						2	5.721	0.308		1670	0					3	3.341	0.425	0.730
							6.117	0.484									3.580	0.286	
1063	2	2.842	0.229	0.143	4	2	3.161	0.262	0.586								3.762	0.203	
		6.268	0.340	0.170			3.434	0.284								5	4.253	0.354	
						2	3.767	0.320									4.255	0.234	
							4.040	0.366									4.650	0.355	
						2	4.786	0.373									5.051	0.332	
							4.791	0.270									5.426	0.419	
						3	5.416	0.297								2	6.100	0.248	
							5.795	0.460									6.303	0.314	
							5.753	0.173		1733	4	2.870	0.315	0.162	3	4	3.287	0.265	0.312
1095	3	3.811	0.266	0.193	2	2	2.857	0.318	0.290			5.187	0.287	0.224			3.482	0.125	
		4.164	0.365	0.190			3.013	0.278				5.463	0.245	0.164			3.653	0.276	
		6.110	0.602	0.320		2	5.308	0.332				6.250	0.368	0.192			3.512	0.287	
							5.446	0.348								2	4.201	0.198	
1140	1	5.360	0.274	0.205	4	2	2.850	0.245	0.667								4.276	0.297	
							3.010	0.238								2	4.624	0.256	
						3	3.514	0.269									4.900	0.309	
							3.752	0.399									2.862	0.280	
							4.220	0.548		1700	2	5.447	0.261	0.186	4	2	3.083	0.175	0.333
							4.644	0.543				5.010	0.327	0.169			4.225	0.308	
						2	5.004	0.176								2	4.249	0.220	
							6.112	0.419								3	4.631	0.345	
							6.312	0.225									4.999	0.391	
1180	2	5.226	0.244	0.162	3	2	3.540	0.473	0.385							2	4.748	0.093	
		5.317	0.299	0.244			3.870	0.199									5.810	0.327	
						2	4.235	0.424									6.206	0.404	
							4.553	0.254									4.636	0.709	0.102
							5.055	0.271		1813	3	2.386	0.367	0.191	1	2	4.904	0.327	
							6.320	0.258				3.466	0.450	0.240					
							7.403	0.316	0.174			4.184	0.504	0.267					
1223	6	3.844	0.197	0.100	1	3	3.194	0.263				5.430	0.420	0.224					
		4.233	0.374	0.195			3.473	0.294				5.830	0.374	0.195					
		4.604	0.257	0.180						1858	6					2	2.872	0.311	0.934

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(k) Test fluid, methanol; run 63-7-2-2

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles					
	Sites	Bubble center	Bubble width	Area frac-tion, ϕ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, ϕ_m		Sites	Bubble center	Bubble width	Area frac-tion, ϕ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, ϕ_m	
		(a)	(a)				(a)	(a)				(a)	(a)				(a)	(a)		
0	1	3.421	0.225	0.241	4	3	3.770 3.902 4.008	0.182 0.131 0.171	0.571							4.411 4.679 5.287	0.221 0.315 0.227			
						2	4.326 4.563	0.250 0.236							3	5.487 5.662 5.990	0.172 0.179 0.273			
						2	4.942 5.235	0.375 0.260							2	5.046 5.741 5.902	0.162 0.179 0.143	0.579		
						4	5.592 5.753 5.857	0.155 0.204 0.150		489	1	3.420	0.254	0.174	3	3	4.100 4.496 4.686	0.252 0.203 0.177		
							6.018 5.429	0.205 0.240							4	4.496 4.885 5.155	0.203 0.221 0.318			
30	1	3.873	0.216	0.222	4	2	3.437 4.262 4.334	0.156 0.700 0.232	0.582						2	5.711 5.970	0.315 0.303			
						4	4.522 5.010 5.041	0.144 0.155 0.170		519	1	6.005	0.223	0.250	1	11	3.456 3.725 3.918	0.292 0.246 0.140	0.798	
							5.277 5.267 5.723	0.306 0.195 0.239									4.161 4.459 4.578	0.367 0.248 0.236		
						3	5.944 6.046	0.203 0.148									4.753 5.004	0.228 0.275		
80	1	3.443	0.239	0.163	3	3	4.007 4.338 4.557	0.198 0.264 0.174	0.628								5.163 5.411 5.661	0.242 0.255 0.244		
						4	5.162 5.218 5.391	0.204 0.225 0.249		564	3	3.465 4.405 4.968	0.319 0.320 0.148	0.222 0.222 0.104	2	2	3.765 3.986 5.759	0.158 0.285 0.290	0.280	
						4	5.608 5.740 5.863	0.133 0.175 0.230		601	2	4.013 4.436	0.224 0.232	0.239 0.256	3	2	5.992 3.388 3.459	0.261 0.154 0.296	0.303	
							6.029 4.306	0.175 0.288							2	2	4.936 4.958	0.178 0.133		
120	2	3.507 3.656	0.337 0.155	0.271 0.112	2	5	4.546 4.716 4.977	0.193 0.169 0.353	0.435						3		5.840 5.971 6.049	0.204 0.196 0.152		
							4.977 5.304	0.353 0.301		653	4	3.421 3.770	0.226 0.220	0.243 0.231	2	2	4.209 4.356	0.133 0.161	0.191	
						2	5.922 6.058	0.159 0.148									5.664 5.803	0.169 0.157		
160	1	3.458	0.289	0.200	1	16	3.849 4.021 4.245	0.169 0.215 0.279	0.845						3	2	6.009 3.436 3.657	0.255 0.248 0.195	0.701	
							4.234 4.485 4.481	0.154 0.180 0.234		685	0					4		4.203 4.395	0.135 0.248	
							4.665 4.749	0.238 0.256										4.897 5.205	0.185 0.430	
							5.000 5.219	0.246 0.193							5		5.566 5.823	0.292 0.223		
							5.448 5.624 5.763	0.265 0.153 0.124		715	2	3.452	0.284	0.196	3	4	6.030 3.838	0.191 0.172	0.471	
							5.753	0.246												

								5.857	0.177			5.502	0.211	0.212		4.028	0.209			
								6.034	0.176							4.202	0.137			
175	2	3.450	0.275	0.189	3	4		4.323	0.209	0.540						4.373	0.270			
		3.877	0.168	0.134				4.461	0.162							4.950	0.220			
								4.523	0.255							5.182	0.237			
						2		4.754	0.206							5.757	0.190			
								5.031	0.170							5.877	0.208			
								5.063	0.234							5.975	0.194			
						6		5.291	0.135		754	5	3.463	0.310	0.215	1	4	5.430	0.227	J.183
								5.354	0.127				3.905	0.390	0.244			5.670	0.232	
								5.492	0.148				4.233	0.163	0.127			5.870	0.161	
								5.574	0.195				4.435	0.197	0.117			6.010	0.106	
								5.798	0.253				5.177	0.193	0.177					
								6.021	0.193											
240	3	3.443	0.276	0.190	2	2		3.731	0.240	0.666	799	2	3.501	0.326	0.227	2	2	4.464	0.333	J.095
		5.659	0.173	0.143				3.947	0.240				3.873	0.240	0.197			4.467	0.147	
		6.018	0.205	0.200		8		4.291	0.328									4.924	0.271	
								4.460	0.239									5.121	0.201	
								4.649	0.214									5.215	0.315	
								4.835	0.158									5.486	0.226	
								4.861	0.250									5.651	0.255	
								5.057	0.227									5.700	0.236	
								5.298	0.254									5.776	0.304	
								5.269	0.228									6.031	0.194	
270	3	3.470	0.251	0.172	3	2		4.301	0.237	0.359	833	5	3.475	0.307	0.213	1	3	3.563	0.174	J.171
		3.799	0.353	0.246				4.494	0.183				3.907	0.235	0.162			5.790	0.280	
		5.280	0.153	0.112		2		4.839	0.152				4.547	0.372	0.274			6.031	0.203	
								4.995	0.161				4.951	0.117	0.065					
						3		5.712	0.260				5.215	0.184	0.161					
								5.878	0.200											
								6.007	0.240											
325	2	3.447	0.272	0.187	2	4		3.804	0.292	0.583								3.394	0.259	J.562
		4.947	0.261	0.179				4.062	0.343									3.915	0.178	
								4.333	0.199									4.639	0.371	
								4.484	0.226									4.951	0.257	
						7		5.223	0.198									5.211	0.208	
								5.428	0.213									5.720	0.336	
								5.542	0.221									5.003	0.225	
								5.661	0.169									3.414	0.215	J.703
								5.797	0.159									3.486	0.353	
								5.900	0.137									3.765	0.366	
								6.044	0.191									4.023	0.177	
								3.742	0.265	0.385								4.352	0.276	
365	3	3.433	0.245	0.167	2	5		3.839	0.200									4.502	0.255	
		4.932	0.256	0.175				4.067	0.319	0.385								4.758	0.162	
		5.600	0.170	0.130				4.354	0.255									4.936	0.195	
								4.516	0.106									5.563	0.160	
						2		5.924	0.161									5.703	0.152	
								6.035	0.174									5.881	0.205	
								3.799	0.217	0.420								6.056	0.144	
400	3	3.462	0.250	0.171	3	3		3.889	0.339									3.812	0.242	J.375
		4.958	0.191	0.174				4.047	0.186									4.041	0.251	
		5.546	0.411	0.288		3		4.323	0.220									4.511	0.289	
								4.505	0.145									5.670	0.174	
								4.681	0.207									5.834	0.179	
						2		5.482	0.230		1001	5	3.440	0.310	0.215	1	5	5.430	0.166	J.203
								6.072	0.116				3.846	0.257	0.170			5.608	0.191	
								3.512	0.311	0.672			4.252	0.229	0.250			5.762	0.231	
443	1	4.994	0.222	0.235	3	6		3.838	0.361				4.673	0.256	0.175			5.959	0.163	
								4.062	0.106				4.975	0.192	0.170			6.047	0.155	
								4.208	0.186		1033	3	3.411	0.219	0.228	2	4	3.742	0.213	J.370
													4.887	0.262	0.180			3.721	0.145	

*2.815 movie analyzer units equal 0.75 inch; left end reading 3.310; right end reading, 6.123.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(k) Concluded. Test fluid, methanol; run 63-7-2-2

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles											
	Sites	Bubble center	Bubble width	Area frac-tion, Φ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, Φ_m		Sites	Bubble center	Bubble width	Area frac-tion, Φ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, Φ_m							
	(a)	(a)	(a)			(a)	(a)				(a)	(a)	(a)		(a)	(a)										
1003	3	3.456 4.964 5.455	0.308 0.127 0.209	0.214 0.077 0.208	2	4	4.086	0.184	0.375	1670	2	3.460 5.674	0.329 0.135	0.227 0.083	4	2	4.773	0.277	0.392							
							4.302	0.249									5.081	0.238								
							5.453	0.209									5.629	0.209								
							5.662	0.208									5.719	0.161								
							5.849	0.167									5.923	0.246								
							6.026	0.187									3.875	0.273								
							3.764	0.222									4.077	0.151								
							4.002	0.254									4.315	0.212								
							4.235	0.213									4.460	0.271								
							4.372	0.280									4.872	0.174								
1095	6	3.455 4.383 4.944 5.406 5.641 5.999	0.277 0.264 0.173 0.183 0.162 0.235	0.191 0.181 0.143 0.160 0.125 0.175	1	2	4.009	0.181	0.412	1733	2	3.428 4.432	0.233 0.210	0.257 0.210	2	2	3.865	0.317	0.613							
							5.777	0.181									4.136	0.224								
							5.767	0.219									4.748	0.243								
							5.969	0.181									4.924	0.141								
							3.777	0.181									5.065	0.159								
							4.009	0.282									5.171	0.177								
																	5.450	0.380								
																	5.687	0.215								
																	5.820	0.180								
																	5.004	0.243								
1140	4	4.397 4.985 5.659 6.025 4.397 4.921 5.661	0.253 0.215 0.147 0.210 0.242 0.273 0.187	0.175 0.175 0.105 0.210 0.165 0.185 0.170	1	3	3.460	0.297	0.257	1766	1	3.997 0.254	0.174	4	2	3.373	0.121	0.614								
							3.760	0.302								3.422	0.218									
							3.760	0.236								3.788	0.302									
																3.951	0.350									
																4.110	0.263									
																4.353	0.223									
																4.912	0.130									
																5.089	0.225									
																5.414	0.214									
																5.630	0.219									
1223	3	3.447 4.427 4.977	0.265 0.231 0.143	0.182 0.172 0.397	2	2	3.735	0.220	0.477	1813	1	3.436	0.187	0.167	3	4	3.474	0.326	0.691							
							4.037	0.388									3.741	0.209								
							5.362	0.234									3.956	0.221								
							5.660	0.313									4.177	0.221								
							5.967	0.304									4.445	0.203								
							3.796	0.313									4.677	0.260								
							4.367	0.352									4.718	0.223								
							5.335	0.236									5.144	0.223								
							5.564	0.232									5.593	0.242								
							5.785	0.210									5.940	0.253								
1311	2	4.901 5.985	0.217 0.274	0.224 0.189	2	2	3.427	0.253	0.357	1828	1	6.154	0.126	3	5	3.445	0.143	0.567								
							3.657	0.285								3.702	0.266									
							3.778	0.117								3.834	0.212									
							3.893	0.176								3.878	0.177									
							4.121	0.286								4.072	0.305									
							4.312	0.188								4.382	0.117									
							4.377	0.287								4.360	0.086									
							4.562	0.267								5.117	0.228									
							5.194	0.227								5.367	0.161									
							5.362	0.191								5.467	0.195									
1377	1	3.901	0.334	0.235	2	5	3.537	0.270	0.397																	
							4.078	0.273																		
							4.316	0.317																		
							4.577	0.263																		
							4.777	0.133																		
							4.923	0.158																		
							5.097	0.195																		
							5.262	0.157																		

						2	3.755	0.278								5.816	0.213	
							6.017	0.247								3.804	0.346	0.564
1411	3	3.466	0.327	0.227	2	2	4.327	0.204	J.238	1890	3	3.446	0.278	0.192	2	4	4.144	0.334
		3.893	0.278	0.192			4.543	0.229				4.938	0.239	0.163			4.409	0.196
		4.956	0.137	0.089		3	5.717	0.179				5.291	0.195	0.181			4.645	0.277
							5.864	0.154								3	5.578	0.261
							6.026	0.224									5.736	0.197
1441	2	3.472	0.303	0.210	4	3	3.889	0.301	0.581								5.977	0.284
		5.671	0.158	0.119			4.162	0.245		1927	2	3.458	0.287	0.198	3	3	4.135	0.271
							4.320	0.158				3.876	0.175	0.146			4.360	0.179
						2	4.870	0.290									4.536	0.173
							4.937	0.094									4.894	0.202
						2	5.187	0.180								2	5.102	0.214
							5.325	0.388									5.544	0.101
						2	5.986	0.289								4	5.600	0.091
							6.034	0.194									5.758	0.232
1486	1	3.433	0.256	0.175	2	8	3.862	0.209	3.464								5.989	0.231
							4.004	0.075		1965	1	3.449	0.275	0.189	4	3	3.964	0.324
							4.103	0.122									4.201	0.150
							4.239	0.151									4.370	0.188
							4.425	0.220								2	4.735	0.115
							4.702	0.334									5.094	0.202
							4.935	0.133								2	5.518	0.257
							5.106	0.209									5.674	0.185
						2	5.829	0.286								2	5.948	0.172
							6.054	0.165									6.034	0.177
1521	3	3.472	0.326	0.227	1	6	3.872	0.365	0.489	2000	5	3.443	0.268	0.184	1	4	5.341	0.352
		5.321	0.208	0.206			3.884	0.269				3.892	0.151	0.107			5.621	0.208
		5.966	0.319	0.222			4.117	0.125				4.091	0.090	0.039			5.812	0.174
							4.308	0.256				4.450	0.238	0.162			6.003	0.208
							4.600	0.328				4.797	0.153	0.112				
							4.905	0.282				3.410	0.217	0.224	2	6	3.725	0.210
1571	0				2	2	3.426	0.237	0.870	2029	2	5.929	0.350	0.244			3.885	0.110
							3.489	0.363									3.939	0.158
						10	3.925	0.253									4.052	0.224
							4.134	0.265									4.247	0.166
							4.372	0.211									4.499	0.338
							4.563	0.170								3	4.394	0.214
							4.728	0.160									5.101	0.201
							4.935	0.254									5.314	0.225
							5.235	0.346									5.728	0.186
							5.608	0.400		2069	3	3.407	0.191	0.174	1	8	3.912	0.183
							5.856	0.225				5.582	0.155	0.114			4.069	0.178
							6.049	0.160				5.970	0.302	0.209			4.268	0.221
1600	1	3.485	0.347	0.242	3	6	3.860	0.193	0.539								4.518	0.279
							4.007	0.101									4.808	0.300
							4.136	0.156									5.075	0.235
							4.312	0.197									5.229	0.154
							4.495	0.163									5.518	0.369
							4.700	0.242		2117	6	3.890	0.128	0.073	2	2	3.492	0.317
						3	5.015	0.180				4.117	0.203	0.196			4.387	0.095
							5.357	0.169				4.937	0.154	0.113	2		4.534	0.334
							5.237	0.190				5.270	0.133	0.084				
						4	5.476	0.115				5.600	0.273	0.187				
							5.672	0.273		2152	7	5.994	0.247	0.169				
							5.897	0.257				3.487	0.247	0.169	1	2	5.944	0.204
							6.065	0.166				5.795	0.176	0.148			6.058	0.147
1646	1	3.446	0.249	0.200	3	2	3.873	0.173	0.535			4.107	0.191	0.174				
							4.061	0.202				4.387	0.210	0.210				
						4	4.303	0.164				4.959	0.182	0.153				
							4.460	0.249				5.270	0.153	0.117				
											5.636	0.205	0.200					

Total number of sample frames, k, 55.
Total number of single bubbles, h, 135.
Total number of merging bubbles, 447.
Average instantaneous bubble population, n_{av} , 10.58.
Average area fraction of influence of single bubble, $\phi_{s,av}$, 0.182.
Average area fraction of merging bubbles, $\phi_{m,av}$, 0.4704.
Standard deviations associated with $\phi_{m,av}$, 0.1833.

^a2.813 movie analyzer units equal 0.75 inch; left end reading, 3.310; right end reading, 6.123.

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(1) Test fluid, methanol; run 63-7-8-1

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m		Sites	Bubble center	Bubble width	Area fraction, φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, φ_m
	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)		(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)
0	2	3.244 3.736	0.133 0.262	0.081 0.283	2	3	3.004 3.326 3.567 3.770 3.868	0.263 0.380 0.103 0.216 0.148	0.280	715	5	3.253 3.358 4.543 3.458 3.946	0.077 0.083 0.117 0.221 0.114	0.025 0.029 0.058 0.206 0.055	1	2	4.820 5.012	0.155 0.229	0.083
50	2	4.408 3.770	0.268 0.123	0.183 0.070	1	2	3.249 3.475	0.166 0.286	0.113	754	7	3.253 3.661 4.533 4.839 5.006 5.453 5.883	0.067 0.234 0.207 0.192 0.078 0.172 0.163	0.019 0.230 0.180 0.097 0.026 0.125 0.112	0				
100	3	3.252 4.097 4.813 4.984 3.457	0.071 0.124 0.079 0.038 0.204	0.021 0.065 0.026 0.038 0.204	0					799	4	3.270 4.241 4.975 5.426	0.082 0.257 0.205 0.271	0.028 0.278 0.177 0.185	0				
125	2	3.264 4.475	0.095 0.162	0.038 0.110	2	2	3.462 3.705 3.268 3.450 3.553 3.689 3.767 3.904	0.253 0.232 0.288 0.128 0.177 0.132 0.124 0.146	0.316	833	5	3.238 3.607 4.093 4.996 5.957	0.058 0.319 0.093 0.187 0.046	0.014 0.221 0.036 0.147 0.009	0				
160	6	3.257 4.113 4.823 5.000 3.745 3.590	0.081 0.230 0.095 0.180 0.176 0.287	0.028 0.223 0.036 0.136 0.130 0.199	1	2	3.883 3.905	0.114 0.143	0.035	927	3	3.267 3.890 4.452	0.113 0.066 0.236	0.054 0.015 0.234	3	2	3.712 3.708 4.039 4.036 5.816 5.929	0.255 0.107 0.213 0.070 0.203 0.127	0.215
195	7	3.253 3.618 4.245 4.578 4.992 5.546 5.897	0.143 0.207 0.225 0.347 0.106 0.186 0.123	0.080 0.180 0.213 0.241 0.047 0.146 0.064	0					958	4	3.262 3.702 3.475 3.907	0.105 0.064 0.139 0.136	0.046 0.017 0.081 0.078	0				
240	3	3.311 4.994 3.868	0.093 0.134 0.223	0.036 0.076 0.209	0					1001	2	4.831 3.446	0.127 0.176	0.066 0.130	1	2	3.325 3.547	0.204 0.231	0.137
270	4	3.586 4.982 3.341 3.443	0.391 0.218 0.070 0.066	0.273 0.200 0.021 0.018	2	2	3.244 3.303 3.561 3.602	0.087 0.113 0.111 0.192	0.073	1033	4	3.276 4.994 3.455 3.903	0.098 0.168 0.100 0.170	0.040 0.114 0.042 0.122	0				
										1063	2	3.272 3.946	0.090 0.076	0.034 0.024	2	2	3.809 4.047 5.373	0.239 0.291 0.266	0.344

325	5	3.261	0.150	0.095	0												5.667	0.375	
		4.116	0.075	0.024					10.75	3	3.307	0.151	0.096	2	2		4.827	0.163	0.075
		5.001	0.142	0.087							3.687	0.177	0.133				4.980	0.166	
		5.455	0.149	0.093							4.102	0.136	0.080		2		5.791	0.090	
		5.890	0.173	0.120													5.387	0.102	
365	3	3.305	0.093	0.036	2	2	4.810	0.154	5.230	1140	3	3.747	0.113	0.054	2	2	3.243	0.083	0.262
		5.206	0.128	0.067			5.018	0.232				4.103	0.229	0.221			3.329	0.088	
		5.866	0.162	0.110		3	5.310	0.239				3.720	0.113	0.054		3	4.830	0.120	
							5.554	0.137									4.759	0.282	
							5.697	0.064									5.323	0.446	
400	3	3.248	0.070	0.021	0												3.266	0.121	0.197
		5.210	0.163	0.112													3.362	0.127	
		5.791	0.342	0.238													3.717	0.147	
443	4	3.269	0.116	0.057	1	3	5.699	3.101	5.640								3.804	0.204	
		3.637	0.384	0.268			5.783	3.102									3.739	0.187	
		4.116	0.239	0.240			5.761	0.157									4.003	0.240	
		4.995	0.097	0.040															
489	2	4.850	0.139	0.081	1	2	3.610	3.186	5.392	1223	7	3.647	0.086	0.031	0				
		5.934	0.117	0.050			3.799	3.230				3.670	0.100	0.117					
519	2	3.269	0.107	0.048	1	3	3.782	0.111	5.077			4.255	0.247	0.257					
		4.837	0.143	0.080			3.900	0.180				4.077	0.324	0.224					
							3.999	3.174				4.077	0.103	0.141					
												3.680	0.124	0.067					
564	6	3.263	0.032	0.030	1	2	4.304	3.332	5.157	1201	5	3.647	3.263	0.271					
		4.842	0.194	0.150			4.527	0.135				3.660	0.161	0.107	1	3	4.580	0.307	0.161
		4.988	0.073	0.022								3.623	0.175	0.127			4.849	0.218	
		5.297	0.414	0.290								3.711	0.140	0.083			4.787	0.123	
		5.577	0.096	0.037								3.237	0.067	0.017	2	2	3.573	0.207	0.167
		5.857	0.117	0.058								4.400	0.243	0.247			3.717	0.271	
601	4	3.263	0.102	0.044	1	2	3.809	0.107	5.020			4.770	0.067	0.020		2	3.827	0.174	
		3.965	0.140	0.083			3.966	3.387									3.723	0.116	
		5.448	0.075	0.024													3.305	0.067	0.264
		5.593	0.153	0.097													3.473	0.200	
653	6	3.295	0.157	0.097	0												3.513	0.203	
		3.607	0.174	0.127													3.711	0.202	
		4.411	0.097	0.040													3.837	0.224	
		5.007	0.076	0.024													3.245	0.207	0.177
		5.484	0.085	0.030													3.367	0.121	
		5.938	0.103	0.045													3.430	0.122	
683	6	3.275	0.177	0.132	1	2	3.327	0.135	3.063								4.370	0.240	
		4.405	0.033	0.030			3.448	0.147		1441	4	3.260	0.120	0.061	0		3.257	0.319	
		4.547	0.044	0.037								4.397	0.093	0.027					
		4.850	0.139	0.081								5.731	0.134	0.070					
		5.023	0.154	0.100															
		5.742	0.075	0.024															

^a3.194 movie analyzer units equal 0.75 inch; left end reading, 3.180; right end reading, 6.374 (average right limit, 5.984; reduced area of strip evaluated because of obscuration of film).

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(2) Concluded. Test fluid, methanol; run 63-7-8-1

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area frac-tion, Φ_s	Sites	Number of merging bubbles	Site center	Site width	Area frac-tion, Φ_m		Sites	Bubble center	Bubble width	Area frac-tion, Φ_s	Sites	Number of merging bubbles	Site center	Site width	Area frac-tion, Φ_m
	(a)	(a)			(a)	(a)					(a)	(a)			(a)	(a)			
1486	2	4.270 5.945	0.246 0.091	0.255 0.035	1	3	3.207 3.265 3.349	0.037 0.078 0.090	0.010						2		3.576 3.589 3.875 3.868 4.060 4.044	0.205 0.231 0.198 0.204 0.180 0.140	
1521	5	3.259 4.088 4.488 4.990 5.302	0.108 0.188 0.211 0.125 0.213	0.049 0.149 0.187 0.066 0.191	0					2192	3	4.502 5.299 5.916	0.150 0.431 0.110	0.095 0.302 0.051	3	2	3.203 3.257 3.755 3.749 4.724 4.877	0.076 0.083 0.264 0.275 0.222 0.216	0.267
1571	4	3.554 4.125 4.823 4.795	0.318 0.225 0.168 0.117	0.220 0.213 0.119 0.058	2	2	3.253 3.304 3.751 3.895	0.074 0.097 0.175 0.192	0.087							2	3.755 3.749 4.724 4.877	0.264 0.275 0.222 0.216	
1600	4	3.503 4.511 4.990 5.275	0.106 0.229 0.136 0.240	0.047 0.221 0.078 0.242	3	2	3.245 3.328 3.896 4.157 5.647 5.792 5.902	0.082 0.085 0.318 0.309 0.270 0.152 0.155	0.333	2237	3	3.225 3.743 4.819	0.100 0.097 0.077	0.042 0.040 0.025	1	3	3.213 3.299 3.328 3.621 3.763 4.066 4.319	0.144 0.183 0.125 0.186 0.190 0.217 0.326	0.074
1640	5	3.252 3.367 3.874 4.460 5.593	0.076 0.084 0.142 0.183 0.189	0.024 0.030 0.085 0.141 0.150	2	2	4.798 4.963 5.857 5.952	0.214 0.235 0.138 0.075	0.132	2317	4	3.217 3.700 4.813 5.883	0.068 0.116 0.107 0.153	0.019 0.057 0.048 0.099	0				
1690	3	3.641 5.844 5.963	0.330 0.100 0.043	0.227 0.042 0.008	2	2	3.248 3.304 4.838 4.986 5.220 5.291 5.568	0.086 0.087 0.197 0.237 0.364 0.138 0.417	0.391	2347	3	3.646 4.504 5.893	0.234 0.190 0.175	0.230 0.152 0.129	2	2	3.200 3.349 4.974 5.324 5.420 5.626 5.690	0.135 0.254 0.312 0.388 0.313 0.217 0.166	0.484
1733	5	3.704 4.480 4.993 5.343 5.967	0.131 0.145 0.086 0.110 0.060	0.072 0.087 0.031 0.051 0.015	3	2	3.265 3.308 3.850 3.882 5.393 5.530	0.114 0.127 0.153 0.157 0.141 0.229	0.157	2397	0	3.238 3.603 4.530 4.980 5.694 5.938	0.119 0.120 0.169 0.173 0.155 0.101	0.060 0.061 0.120 0.120 0.101 0.043	0				
1766	4	3.672 4.311 4.775	0.151 0.107 0.164	0.096 0.043 0.113	1	2	3.215 3.309	0.074 0.115	0.020	2437	5	3.237 4.068 4.521 4.971	0.107 0.168 0.217 0.151	0.048 0.119 0.198 0.090	1	2	5.494 5.601	0.141 0.112	0.034

1813	4	3.43	0.100	0.042	1	3	4.582	0.374	0.192	2473	4	5.305	0.204	0.175	1	2	3.260	0.100	0.023
		3.264	0.131	0.072			4.343	0.148				3.950	0.442	0.230			3.318	0.108	
		3.660	0.243	0.261			5.320	0.219				4.830	0.102	0.044					
		3.663	0.202	0.172								5.467	0.263	0.291					
		3.973	0.133	0.074								5.920	0.121	0.062					
1858	3	4.121	0.245	0.253	3	2	3.234	0.145	0.132	2516	3	4.311	0.242	0.247	3	2	3.216	0.067	0.209
		4.530	0.241	0.244			3.339	0.137				4.982	0.135	0.077			3.293	0.087	
		3.24	0.177	0.132		2	3.633	0.113				5.942	0.084	0.030	2		3.876	0.167	
						2	3.756	0.238							3		4.033	0.146	
							3.726	0.041									5.305	0.252	
							3.780	0.067									5.430	0.135	
1890	3	3.367	0.300	0.207	0					2551	2	4.311	0.140	0.083	3	2	3.245	0.086	0.162
		3.624	0.128	0.067								4.024	0.135	0.077			3.338	0.189	
		4.023	0.215	0.190											3		3.998	0.084	
		4.602	0.125	0.065													4.026	0.074	
		4.381	0.131	0.072													4.084	0.210	
		3.233	0.135	0.144											2		3.854	0.206	
		3.550	0.234	0.230													3.928	0.108	
		3.964	0.067	0.010													3.991	0.126	0.041
1777	4	4.981	0.122	0.003	1	2	3.246	0.120	0.04	2584	4	3.312	0.244	0.251	1	2	3.991	0.126	0.041
		3.231	0.230	0.223			3.495	0.172				4.380	0.153	0.099			4.130	0.153	
		3.54	0.175	0.160								3.457	0.224	0.211					
		3.933	0.110	0.059								3.857	0.186	0.149					
1963	2	4.277	0.318	0.220	2	2	3.227	0.115	0.224	2624	3	3.277	0.203	0.173	0				
		3.060	0.108	0.049		3	3.360	0.185				3.607	0.278	0.190					
							3.612	0.262				4.871	0.134	0.070					
							3.737	0.232				3.564	0.184	0.143					
							3.880	0.208				3.852	0.221	0.206					
2000	3	3.242	0.103	0.045	1	2	3.558	0.278	0.165	2673	3	3.238	0.121	0.062	0				
		4.987	0.152	0.097			3.602	0.289				3.743	0.310	0.220					
		3.875	0.213	0.191								4.631	0.137	0.077					
2027	3	3.211	0.102	0.044	0							3.605	0.140	0.083					
		3.601	0.329	0.223								3.923	0.139	0.081					
		4.382	0.185	0.144								4.815	0.128	0.069	2	2	3.681	0.189	0.191
		3.584	0.235	0.232								3.000	0.138	0.080			3.789	0.240	
		3.808	0.138	0.080								3.253	0.237	0.236	2		4.080	0.121	
2063	2	3.212	0.095	0.038	0							3.610	0.144	0.087			4.255	0.272	
		3.928	0.108	0.049								3.230	0.112	0.053	2	2	4.430	0.173	0.074
2117	4	3.220	0.122	0.063	0							3.745	0.088	0.033			4.504	0.138	
		3.636	0.321	0.222								3.215	0.193	0.157	2		3.855	0.141	
		4.283	0.407	0.212								3.690	0.088	0.033			3.952	0.071	
		4.493	0.141	0.084								3.221	0.090	0.039	1	3	3.596	0.153	0.062
2132	1	4.833	0.199	0.167	3	2	3.230	0.195	0.345	2790	2	3.940	0.105	0.040			3.733	0.121	
							3.312	0.248									3.866	0.144	

Total number of sample frames, k , 70.
 Total number of single bubbles, n , 263.
 Total number of merging bubbles, 196.
 Average instantaneous bubble population, n_{av} , 6.56.
 Average area fraction of influence of single bubble, $\phi_{s,av}$, 0.109.
 Average area fraction of merging bubbles, $\phi_{m,av}$, 0.1099.
 Standard deviation associated with $\phi_{m,av}$, 0.1173.

^a3.194 movie analyzer units equal 0.75 inch; left end reading, 3.180; right end reading, 6.374 (average right limit, 5.984; reduced area of strip evaluated because of obscuration of film).

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(m) Test fluid, methanol; run 63-7-8-4

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area fraction, Φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, Φ_m		Sites	Bubble center	Bubble width	Area fraction, Φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, Φ_m
	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)		(a)	(a)	(a)	(a)	(a)	(a)	(a)	(a)	
0	4	3.231 3.455 4.091 4.771	0.207 0.144 0.163 0.054	0.173 0.086 0.116 0.012	2	2	3.710 3.833 3.880 5.559 5.786	0.120 0.207 0.199 0.186 0.269	0.212	601	1	5.416	0.174	0.126	4	2	5.766 3.150 3.263 3.611 3.743 4.809 4.951	0.377 0.082 0.144 0.126 0.138 0.167 0.158	0.249
30	1	4.720	0.353	0.243	3	2	3.245 3.450 4.057 4.253 5.387 5.567 5.662 5.785 5.818	0.128 0.283 0.209 0.309 0.170 0.161 0.148 0.191 0.241	0.416	653	0			4	2	5.668 5.761 3.225 3.391 3.929 4.142 4.595	0.165 0.326 0.145 0.186 0.261 0.329 0.229	0.403	
60	1	3.221	0.142	0.084	4	3	3.538 3.671 3.855 4.422 4.606 4.872 5.412 5.582 5.836 5.872	0.230 0.242 0.263 0.007 0.360 0.255 0.369 0.271 0.173 0.101	0.605	665	0			3	3	4.770 5.611 5.804 3.210 3.278 3.453 3.694 3.814 4.594 4.781	0.184 0.139 0.246 0.129 0.177 0.172 0.170 0.237 0.302 0.205	0.637	
120	2	3.704 4.604	0.184 0.171	0.141 0.122	3	2	3.219 3.404 4.775 4.925 5.185 5.653 5.771 5.863	0.134 0.237 0.068 0.278 0.243 0.147 0.146 0.149	0.304	715	3	3.208 4.297 4.784	0.207 0.066 0.092	0.178 0.018 0.035	3	4	4.982 5.324 5.603 5.843 3.418 3.577 3.819 4.078 4.982 5.140 5.560 5.819	0.380 0.305 0.253 0.226 0.118 0.261 0.223 0.294 0.217 0.180 0.282 0.236	0.446
160	3	4.074 4.144 5.064	0.194 0.154 0.131	0.156 0.099 0.071	2	2	3.243 3.387 3.312 3.257 3.492 5.634 5.839	0.191 0.199 0.313 0.152 0.205 0.203 0.206	0.323	754	0			3	4	3.376 3.497 4.814 4.974 5.099 5.810 5.845	0.105 0.137 0.257 0.188 0.312 0.247 0.222	0.537	
193	2	3.746 4.067	0.154 0.230	0.099 0.220	4	2	3.168 3.271 4.425 4.639 4.931 5.185 5.472 5.652 5.857	0.119 0.130 0.315 0.113 0.292 0.216 0.215 0.219 0.190	0.411	777	1	3.711	0.133	0.074	4	3	3.149 3.257 3.434 4.008 4.214 4.446 4.854 4.996 5.556 5.627 5.855	0.090 0.168 0.212 0.224 0.225 0.233 0.130 0.155 0.170 0.257 0.174	0.428
246	4	3.764 4.420 4.940 5.223	0.165 0.192 0.221 0.164	0.113 0.153 0.203 0.117	2	4	3.213 3.303 3.478 3.674 3.822 3.860 3.672 3.779 3.379	0.162 0.153 0.196 0.197 0.215 0.113 0.111 0.149 0.155	0.254	833	2	3.260	0.230	0.220	4	2	3.714	0.117	0.353

270	2	3.749 3.546	0.184 0.250	0.141 0.260	3	2	3.241 3.385 4.210 4.495 4.721 5.834 5.890	0.105 0.134 0.393 0.164 0.288 0.215 0.122	0.350		3.465	0.097	0.039		2	3.756 4.275 4.485 4.822 5.007 5.515 5.684 5.829	0.133 0.215 0.255 0.125 0.244 0.190 0.148 0.252		
325	1	4.025	0.232	0.224	3	5	3.179 3.289 3.494 3.658 3.693 4.408 4.719 4.928 5.535 5.761	0.113 0.225 0.184 0.145 0.117 0.396 0.227 0.171 0.141 0.358	0.526	885	2	3.225 4.800	0.165 0.080	0.113 0.027	2	3	3.427 3.620 3.893 5.515 5.682 5.857	0.137 0.248 0.298 0.181 0.153 0.196	0.270
365	4	3.696 4.001 4.447 4.905	0.180 0.207 0.303 0.293	0.135 0.176 0.207 0.200	2	3	3.174 3.265 3.417 5.651 5.826	0.126 0.160 0.144 0.125 0.224	0.133	938	0			0.165 0.026 0.023 0.218	2	7	3.218 3.379 3.552 3.712 3.851 4.055 4.237 4.689 4.750 5.097 5.444 5.791	0.187 0.135 0.210 0.110 0.169 0.312 0.295 0.276 0.237 0.456 0.363 0.331	0.832
400	1	4.629	0.137	0.078	4	3	3.181 3.247 3.385 3.881 4.046 4.176 4.313 4.465	0.129 0.152 0.232 0.229 0.184 0.152 0.122 0.357	0.665							5	3.444 3.565 3.567 3.715 5.015 5.181 5.598	0.155 0.387 0.187 0.212 0.252 0.164 0.231	
						2	3.024 3.048 3.442 3.638 3.842	0.166 0.201 0.425 0.212 0.196		1001	3	3.224 4.067 4.753	0.199 0.206 0.096	0.165 0.176 0.038	3	4	3.444 3.565 3.567 3.715 5.015 5.181 5.598	0.155 0.387 0.187 0.212 0.252 0.164 0.231	0.323
443	4	3.202 3.441 4.784 5.833	0.186 0.157 0.108 0.202	0.144 0.102 0.048 0.170	2	2	4.055 4.257 5.413 5.551 5.591	0.244 0.161 0.140 0.136 0.216	0.177	1033	2	3.217 4.358	0.198 0.353	0.163 0.243	4	2	3.680 3.819 4.774 4.806 5.058 5.235 5.625 5.771	0.122 0.157 0.071 0.078 0.190 0.154 0.150 0.291	0.227
487	4	3.194 3.594 4.290 4.776	0.174 0.147 0.261 0.035	0.126 0.090 0.285 0.038	1	3	3.444 5.664 5.860	0.232 0.208 0.185	0.136							2	3.197 3.230 3.721 3.749 5.615 5.843	0.187 0.253 0.191 0.160 0.260 0.196	
519	0				3	2	3.145 3.255 3.656 3.816 4.027 4.284 4.615 4.748 5.357 5.628 5.844	0.103 0.116 0.152 0.221 0.272 0.242 0.420 0.148 0.275 0.267 0.165	0.578	1063	4	3.464 4.262 4.781 5.241	0.120 0.157 0.076 0.164	0.060 0.102 0.024 0.112	3	2	3.197 3.230 3.721 3.749 5.615 5.843	0.187 0.253 0.191 0.160 0.260 0.196	0.278
						3	5.357 5.628 5.844	0.275 0.267 0.165		1095	0				3	7	3.222 3.427 3.523 3.622 3.741 3.874 4.128 4.725 4.942 5.260	0.231 0.177 0.136 0.128 0.157 0.143 0.324 0.126 0.309 0.117	0.555
564	1	4.008	0.179	0.133	3	4	3.210 3.350 3.457 3.603 4.641 4.930 5.409	0.181 0.167 0.147 0.145 0.236 0.342 0.337	0.498							4			

^a3.204 movie analyzer units equal 0.75 inch; left end reading, 3.114; right end reading, 6.317 (average right limit, 5.945; reduced area of strip evaluated because of obscuration of film).

TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(m) Concluded. Test fluid, methanol; run 63-7-8-4

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles					
	Sites	Bubble center	Bubble width	Area fraction, Φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, Φ_m		Sites	Bubble center	Bubble width	Area fraction, Φ_s	Sites	Number of merging bubbles	Site center	Site width	Area fraction, Φ_m	
		(a)	(a)				(a)						(a)	(a)			(a)	(a)		
1140	2	3.848 3.428	0.135 0.083	0.076 0.029	4	2	5.455 5.657 5.833 3.220 3.244 3.474 3.604 3.627 4.703 4.937 5.040 5.139 5.740 5.874 5.813	0.273 0.130 0.222 0.180 0.098 0.202 0.141 0.213 0.300 0.168 0.237 0.135 0.169 0.188 0.310	0.510	1766	2	3.869 4.416	0.335 0.282	0.230 0.192	2	4	3.653 3.788 3.823 4.028 4.136 4.336 4.580 4.608 4.741 4.907 5.402 5.815 5.865 3.160 3.289 3.440 3.503 5.056 5.251 5.534 5.736 5.882 3.448 3.637 3.920 4.198 4.385 4.810 4.951 5.165 5.278 5.587 5.739 5.888 3.202 3.292 3.463 3.715 3.843 4.713 4.828 5.000 5.555 5.768 5.932 4.818 4.758 5.271 5.469 3.657 5.841 5.921 3.135 3.233 3.427 3.689 3.806	0.163 0.167 0.188 0.210 0.210 0.190 0.142 0.115 0.151 0.414 0.577 0.248 0.148 0.390 0.168 0.134 0.103 0.269 0.290 0.276 0.128 0.165 3.150 0.228 0.237 0.319 0.297 0.123 0.226 0.071 0.155 0.198 0.176 0.122 0.117 0.183 0.159 0.125 0.130 0.078 0.153 0.191 0.187 0.238 0.390 0.391 0.270 0.190 0.205 0.171 0.147 0.074 0.087 0.146 0.742 0.133 0.101	0.352	0.507
1180	1	4.052	0.206	0.176	3	6	3.174 3.285 3.413 3.450 3.556 3.672 4.655 4.656 4.818 5.666 5.849 3.188 3.245 3.496 3.681 3.694 3.848 3.988 4.196 5.479 5.754 5.878 3.184 3.248 3.447 3.587 4.012 4.207 4.286 4.481 4.720 5.488 5.703 5.892 3.740 3.852 3.423 5.601 5.755 5.900	0.081 0.116 0.140 0.186 0.171 0.259 0.254 0.182 0.079 0.168 0.198 0.122 0.140 0.216 0.154 0.127 0.180 0.100 0.413 0.391 0.245 0.159 0.122 0.151 0.136 0.144 0.132 0.377 0.159 0.230 0.249 0.328 0.274 0.138 0.133 0.119 0.179 0.234 0.234 0.174 0.116 0.153 0.220	0.355	1813	1	3.238	0.163	0.110	5	2	3.448 3.637 3.920 4.198 4.385 4.810 4.951 5.165 5.278 5.587 5.739 5.888 3.202 3.292 3.463 3.715 3.843 4.713 4.828 5.000 5.555 5.768 5.932 4.818 4.758 5.271 5.469 3.657 5.841 5.921 3.135 3.233 3.427 3.689 3.806	0.163 0.167 0.188 0.210 0.210 0.190 0.142 0.115 0.151 0.414 0.577 0.248 0.148 0.390 0.168 0.134 0.103 0.269 0.290 0.276 0.128 0.165 3.150 0.228 0.237 0.319 0.297 0.123 0.226 0.071 0.155 0.198 0.176 0.122 0.117 0.183 0.159 0.125 0.130 0.078 0.153 0.191 0.187 0.238 0.390 0.391 0.270 0.190 0.205 0.171 0.147 0.074 0.087 0.146 0.742 0.133 0.101	0.507	
1223	1	4.797	0.091	0.034	3	2	3.188 3.245 3.496 3.681 3.694 3.848 3.988 4.196 5.479 5.754 5.878 3.184 3.248 3.447 3.587 4.012 4.207 4.286 4.481 4.720 5.488 5.703 5.892 3.740 3.852 3.423 5.601 5.755 5.900	0.122 0.140 0.216 0.154 0.127 0.180 0.100 0.413 0.391 0.245 0.159 0.122 0.151 0.136 0.144 0.132 0.377 0.159 0.230 0.249 0.328 0.274 0.138 0.133 0.119 0.179 0.234 0.234 0.174 0.116 0.153 0.220	0.522	1858	5	4.805 4.946 5.071 5.545 5.875 3.245 3.251 3.812 4.193 5.243	0.057 0.068 0.073 0.195 0.165 0.090 0.295 0.149 0.395 0.212	0.014 0.019 0.022 0.158 0.113 0.034 0.201 0.092 0.274 0.187	2	3	3.202 3.292 3.463 3.715 3.843 4.713 4.828 5.000 5.555 5.768 5.932 4.818 4.758 5.271 5.469 3.657 5.841 5.921 3.135 3.233 3.427 3.689 3.806	0.163 0.167 0.188 0.210 0.210 0.190 0.142 0.115 0.151 0.414 0.577 0.248 0.148 0.390 0.168		
1261	3				4	2	3.184 3.248 3.447 3.587 4.012 4.207 4.286 4.481 4.720 5.488 5.703 5.892 3.740 3.852 3.423 5.601 5.755 5.900	0.122 0.151 0.136 0.144 0.132 0.377 0.159 0.230 0.249 0.328 0.274 0.138 0.133 0.119 0.179 0.234 0.234 0.174 0.116 0.153 0.220	0.564	1890	5	3.245 3.251 3.812 4.193 5.243	0.090 0.295 0.149 0.395 0.212	0.034 0.201 0.092 0.274 0.187	2	3	3.202 3.292 3.463 3.715 3.843 4.713 4.828 5.000 5.555 5.768 5.932 4.818 4.758 5.271 5.469 3.657 5.841 5.921 3.135 3.233 3.427 3.689 3.806	0.163 0.167 0.188 0.210 0.210 0.190 0.142 0.115 0.151 0.414 0.577 0.248 0.148 0.390 0.168		
1311	4	3.261 3.482 4.332 4.794	0.159 0.090 0.227 0.081	0.109 0.034 0.214 0.027	2	2	3.740 3.852 3.423 5.601 5.755 5.900	0.133 0.119 0.179 0.234 0.174 0.116 0.153 0.220	0.172	1965	1	4.451	0.143	0.085	4	3	3.657 5.841 5.921 3.135 3.233 3.427 3.689 3.806	0.171 0.147 0.074 0.087 0.146 0.742 0.133 0.101	0.456	
1359	1	3.624	0.078	0.025	3	2	3.242 3.429	0.153 0.220	0.361											

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TABLE II. - Continued. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(n) Test fluid, methanol; run 63-7-8-5

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles						
	Sites	Bubble center	Bubble width	Area frac-tion, φ_s	Sites	Number of merging bub-bles	Site center	Site width	Area frac-tion, φ_m		Sites	Bubble center	Bubble width	Area frac-tion, φ_s	Sites	Number of merging bub-bles	Site center	Site width	Area frac-tion, φ_m		
		(a)	(a)				(a)	(a)					(a)	(a)				(a)	(a)		
30	2	3.480 4.630	0.188 0.265	0.144 0.287	2	2	3.151 3.225 3.445 3.581 3.705 3.868 4.139 4.256 4.467 4.526 4.650 4.773 4.888	0.084 0.140 0.135 0.137 0.176 0.151 0.111 0.123 0.299 0.177 0.128 0.118 0.113	0.120						6	3.361 3.629 3.843 4.039 4.665 4.917 4.997 5.193 5.245 5.492 5.826 5.830	0.282 0.254 0.174 0.218 0.279 0.225 0.259 0.239 0.236 0.259 0.271 0.163				
80	4	3.229 3.464 3.714 3.165	0.139 0.191 0.200 0.170	0.079 0.149 0.163 0.118	2	3	4.139 4.256 4.467 5.526 5.650 5.773 5.888	0.111 0.123 0.299 0.177 0.128 0.118 0.113	0.192						2	3.156 3.208 3.944 4.154 4.304 4.703 4.708 4.819 4.909	0.077 0.119 0.176 0.245 0.231 0.206 0.159 0.123 0.104				
120	0				3	5	5.522 5.739 5.899 3.470 3.519 4.760 4.935 5.440 3.724 3.908 3.156 3.233 3.216 3.431 3.567 3.704 3.812 3.901	0.267 0.167 0.152 0.152 0.163 0.144 0.203 0.333 0.235 0.132 0.092 0.148 0.218 0.213 0.141 0.132 0.130 0.141	0.417	564	2	3.470 3.710	0.136 0.190	0.076 0.147	4	2	3.156 3.208 3.944 4.154 4.304 4.703 4.708 4.819 4.909 3.840 4.056 4.948 3.156 3.320 3.479 3.636 3.828 3.150 3.224 3.435 3.746 3.947 4.109 4.380 4.506 4.657 4.849	0.077 0.119 0.176 0.245 0.231 0.206 0.159 0.123 0.104 0.254 0.179 0.211 0.205 0.172 0.147 0.171 0.260 0.095 0.173 0.249 0.373 0.197 0.234 0.194 0.168 0.135 0.248	0.264		
160	1	3.221	0.126	0.065	3	2	3.519 4.760 4.935 5.440 3.724 3.908 3.156 3.233 3.216 3.431 3.567 3.704 3.812 3.901	0.163 0.144 0.203 0.333 0.235 0.132 0.092 0.148 0.218 0.213 0.141 0.132 0.130 0.141	0.291	601	3	3.219 3.463 4.576	0.134 0.205 0.090	0.073 0.172 0.035	2	2	3.840 4.056 4.948 3.156 3.320 3.479 3.636 3.828 3.150 3.224 3.435 3.746 3.947 4.109 4.380 4.506 4.657 4.849	0.254 0.179 0.211 0.205 0.172 0.147 0.171 0.260 0.095 0.173 0.249 0.373 0.197 0.234 0.194 0.168 0.135 0.248	0.338		
195	2	3.465 4.058	0.195 0.348	0.155 0.237	2	2	3.156 3.233 3.216 3.431 3.567 3.704 3.812 3.901	0.092 0.148 0.218 0.213 0.141 0.132 0.130 0.141	0.201						2	6	3.150 3.224 3.435 3.746 3.947 4.109 4.380 4.506 4.657 4.849 3.190 3.285 3.445 3.433 3.600 3.779 3.904	0.095 0.173 0.249 0.373 0.197 0.234 0.194 0.168 0.135 0.248 0.119 0.226 0.198 0.148 0.228 0.130 0.146			
240	2	4.055 4.638	0.186 0.215	0.141 0.189	3	2	3.163 3.237 3.497 3.687 3.781 4.947 3.221	0.086 0.162 0.245 0.220 0.261 0.273 0.275	0.636	685	3	3.714 4.996 3.236	0.177 0.151 0.077	0.126 0.093 0.024	2	3	3.190 3.285 3.445 3.433 3.600 3.779 3.904	0.119 0.226 0.198 0.148 0.228 0.130 0.146	0.226		

							3.221	0.275		715	5	3.183	0.158	0.102	2	2	4.418	0.376	0.296
							3.506	0.294				3.435	0.217	0.192			4.650	0.333	
							5.592	0.125				4.080	0.200	0.165		4	5.507	0.134	
							5.806	0.303				4.962	0.074	0.022			5.638	0.129	
270	1	4.959	0.075	0.023	3	4	3.190	0.108	0.510			5.214	0.179	0.131			5.767	0.128	
							3.282	0.146									5.879	0.142	
							3.472	0.234		754	4	3.841	0.191	0.149	2	3	3.147	0.089	3.222
							3.702	0.227				4.015	0.075	0.023			3.232	0.164	
							4.071	0.162				4.394	0.287	0.193			3.452	0.276	
							4.229	0.398				4.985	0.174	0.124		4	5.511	0.246	
							4.521	0.186									5.677	0.139	
							5.375	0.196									5.814	0.134	
							5.532	0.247									5.928	0.094	
							5.754	0.247		799	5	3.173	0.144	0.085	2	4	3.714	0.289	0.320
							5.917	0.120				3.426	0.194	0.154			3.958	0.198	
325	5	3.183	0.110	0.047	1	4	3.410	0.175	0.115			4.338	0.104	0.044			4.124	0.261	
							5.590	0.185				4.647	0.058	0.014			4.135	0.157	
							5.774	0.182				4.960	0.183	0.137		3	5.544	0.177	
							5.926	0.122									5.707	0.201	
																	5.880	0.145	
365	4	3.189	0.102	0.042	2	4	3.497	0.175	0.278	833	1	3.670	0.231	0.218	3	2	3.220	0.157	0.523
							3.700	0.230									3.378	0.136	
							3.930	0.230								4	4.410	0.318	
							3.991	0.268									4.657	0.240	
							5.646	0.144									4.889	0.273	
							5.802	0.169									5.234	0.417	
							5.906	0.121	0.173							3	5.632	0.203	
400	3	3.508	0.284	0.191	2	2	3.152	0.079									5.843	0.218	
							3.240	0.145									5.890	0.124	
							5.212	0.191		883	6	3.478	0.110	0.049	2	2	3.167	0.121	0.274
							5.381	0.146				3.748	0.137	0.077			3.242	0.184	
							5.547	0.187				4.022	0.161	0.106		5	5.254	0.210	
							5.719	0.156				4.292	0.234	0.224			5.475	0.233	
							5.883	0.173				4.650	0.161	0.106			5.610	0.258	
443	3	4.311	0.299	0.202	4	3	3.137	0.065	0.442			4.942	0.099	0.040			5.751	0.202	
							3.261	0.216									5.911	0.119	
							3.480	0.223									3.156	0.086	3.340
							3.913	0.244		927	1	4.694	0.118	0.057	3	2	3.221	0.126	
							3.974	0.313									3.468	0.259	
							4.828	0.130									3.763	0.331	
							4.994	0.290									4.031	0.205	
							5.628	0.119								4	5.470	0.144	
							5.757	0.139									5.607	0.130	
							5.832	0.135									5.747	0.150	
							5.903	0.153									5.860	0.203	
							5.940	0.080									3.113	0.065	0.259
489	3	3.191	0.145	0.086	2	2	4.974	0.240	0.173	958	2	3.391	0.105	0.045	2	2	3.188	0.114	
							5.230	0.273				3.803	0.336	0.229			5.130	0.229	
							5.757	0.127								4	5.396	0.303	
							5.894	0.146									5.648	0.232	
519	0				3	5	3.182	0.156	0.735								5.867	0.207	

^a5.232 movie analyzer units equal 0.75 inch; left end reading, 3.098; right end reading, 6.330 (average right limit, 5.955; reduced area of strip evaluated because of obscuration of film).

TABLE II. - Concluded. BUBBLE MEASUREMENT FROM MOVIE ANALYZER

[1/16- by 3/4-in. heating strip.]

(n) Concluded. Test fluid, methanol; run 63-7-8-5

Frame	Single bubbles				Merging bubbles					Frame	Single bubbles				Merging bubbles				
	Sites	Bubble center	Bubble width	Area frac-tion, φ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, φ_m		Sites	Bubble center	Bubble width	Area frac-tion, φ_s	Sites	Number of merg-ing bub-bles	Site center	Site width	Area frac-tion, φ_m
	(a)	(a)	(a)		(a)	(a)	(a)	(a)			(a)	(a)	(a)		(a)	(a)	(a)	(a)	
1001	2	3.455 5.377	0.161 0.180	0.106 0.132	3	2 3	3.127 3.190 4.674 4.833 4.954 5.703 5.847	0.046 0.126 0.333 0.189 0.227 0.155 0.206	0.277	1486	2	3.467 4.216	0.122 0.260	0.061 0.276	4	2 2	4.556 5.781 5.902 3.176 3.227 3.738 3.877	0.233 0.146 0.097 0.096 0.185 0.214 0.203	0.535
1033	3	3.448 3.932 4.981	0.220 0.209 0.157	0.198 0.178 0.101	2	2 3	3.157 3.226 5.359 5.635 5.877	0.115 0.148 0.212 0.341 0.143	0.208	1511	2	3.188 4.284	0.100 0.157	0.041 0.101	3	2 3	4.607 4.715 4.898 5.010 5.162 5.411 5.674 5.791 5.892	0.234 0.177 0.327 0.149 0.256 0.243 0.180 0.130 0.119	0.444
1063	2	3.230 4.984	0.170 0.081	0.118 0.027	2	2 4	3.522 3.729 5.436 5.631 5.826 5.950	0.195 0.331 0.159 0.231 0.159 0.120	0.261	1521	2	3.188 4.284	0.100 0.157	0.041 0.101	3	2 2	3.415 3.659 5.011 5.045 5.395 5.642 5.892	0.140 0.348 0.207 0.163 0.140 0.233 0.119	0.444
1095	2	4.427 4.967	0.365 0.170	0.250 0.118	3	2 3 5	3.140 3.200 3.486 3.734 4.047 5.369 5.600 5.735 5.833 5.885	0.093 0.149 0.161 0.335 0.291 0.237 0.225 0.164 0.240 0.136	0.459	1571	3	3.229 3.449 3.714	0.127 0.188 0.165	0.066 0.144 0.111	2	2 3	4.917 5.122 5.482 5.703 5.879 5.518 5.778	0.214 0.196 0.233 0.209 0.144 0.194 0.327	0.207
1140	1	3.485	0.162	0.107	3	2 4 2	3.148 3.230 4.203 4.402 4.546 4.638 5.777 5.888	0.106 0.132 0.345 0.172 0.116 0.178 0.160 0.117	0.328	1600	4	3.243 3.470 3.975 4.949	0.196 0.163 0.245 0.248	0.157 0.108 0.245 0.251	1	2 2	3.518 5.778 3.474 3.684 4.029 4.187	0.194 0.327 0.154 0.266 0.242 0.306	0.130
1180	3	3.188 5.454 5.771	0.114 0.301 0.210	0.053 0.203 0.180	1	6	3.446 3.702 3.712 3.880 4.040 4.262 3.150 3.265 3.475 3.693 3.890	0.205 0.306 0.116 0.117 0.203 0.274 0.095 0.213 0.206 0.230 0.164	0.283	1640	1	3.212	0.168	0.115	3	2 7	3.474 3.684 4.029 4.187 4.611 4.900 5.187 5.404 5.616 5.745 5.875	0.154 0.266 0.242 0.306 0.270 0.356 0.213 0.216 0.209 0.095 0.165	0.614
1223	1	5.851	0.209	0.178	2	7	3.150 3.265 3.475 3.693 3.890	0.095 0.213 0.206 0.230 0.164	0.570	1690	5	4.287 4.604 4.906 5.203	0.248 0.236 0.186 0.145	0.251 0.227 0.141 0.086	3	2 2	3.172 3.224 3.452 3.674	0.089 0.111 0.227 0.216	0.161

							4.078	0.212			5.462	0.278	0.187	2	5.742	0.127		
							4.300	0.233							5.881	0.151		
						4	4.443	0.376	1733	3	3.195	0.129	0.063	2	3.463	0.223	0.261	
							5.214	0.147			4.291	0.129	0.063		3.679	0.208		
							5.364	0.191			4.908	0.233	0.222		3.911	0.256		
							5.436	0.334						3	5.511	0.200		
1261	4	3.481	0.166	0.113	3	2	3.204	0.094	0.222						5.696	0.171		
		3.707	0.157	0.101			3.250	0.132							5.866	0.168		
		3.869	0.100	0.041		3	4.870	0.246	1766	3	3.675	0.068	0.019	2	3.186	0.115	0.201	
		4.442	0.320	0.217			5.033	0.127			3.869	0.172	0.121		3.307	0.131		
							5.148	0.203			4.286	0.304	0.206		3.448	0.147		
						4	5.523	0.141						4	4.688	0.149		
							5.671	0.154							4.831	0.201		
							5.801	0.107							4.983	0.134		
							5.887	0.136							5.120	0.253		
1311	2	3.220	0.167	0.114	3	3	3.667	0.461	0.618	1813	3	3.211	0.177	0.128	3	3.797	0.278	0.312
		4.047	0.215	0.189			3.557	0.182				3.439	0.198	0.160		4.047	0.223	
							3.728	0.160				4.690	0.313	0.212		4.972	0.164	
						3	4.583	0.342								5.176	0.245	
							4.682	0.194							3	5.644	0.202	
							4.910	0.312								5.761	0.195	
						6	5.536	0.274								5.892	0.116	
							5.613	0.203		1858	2	3.209	0.111	0.050	3	3.507	0.294	0.438
							5.708	0.108				4.037	0.229	0.214		3.708	0.109	
							5.825	0.127								3.738	0.216	
							5.887	0.133							2	5.026	0.182	
							5.921	0.065								5.143	0.361	
1359	5	3.193	0.111	0.050	1	4	5.337	0.365	0.180						3	5.574	0.329	
		3.481	0.223	0.203			5.583	0.134								5.766	0.163	
		3.731	0.185	0.140			5.737	0.175								5.887	0.130	
		4.603	0.186	0.141			5.887	0.124		1890	2	3.195	0.135	0.074	3	3.727	0.135	0.372
		4.904	0.234	0.224								3.459	0.273	0.183		3.854	0.198	
1411	1	3.971	0.108	0.048	4	2	3.155	0.077	0.446							4.030	0.154	
							3.236	0.181							2	4.786	0.175	
							3.623	0.237								4.982	0.216	
							3.749	0.214							3	5.300	0.292	
						4	4.460	0.235								5.573	0.254	
							4.593	0.138								5.820	0.241	
							4.693	0.301		1927	1	4.042	0.304	0.206	3	3.202	0.125	0.240
							4.831	0.193								3.353	0.296	
						4	5.562	0.150							2	3.574	0.395	
							5.647	0.149								3.672	0.100	
							5.744	0.191							4	5.403	0.192	
							5.877	0.130								5.586	0.174	
1441	0				3	2	3.176	0.092	0.359							5.762	0.178	
							3.262	0.118								5.898	0.128	
						6	3.486	0.158		1965	2	3.463	0.155	0.098	2	3.123	0.073	0.067
							3.615	0.134				5.748	0.409	0.281		3.213	0.107	
							3.801	0.238							2	4.054	0.126	
							3.967	0.094								4.085	0.188	
							4.227	0.426										

Total number of sample frames, k , 49.
 Total number of single bubbles, n , 124.
 Total number of merging bubbles, 385.
 Average instantaneous bubble population, n_{av} , 10.39.
 Average area fraction of influence of single bubble, $\phi_{s,av}$, 0.156.
 Average area fraction of merging bubbles, $\phi_{m,av}$, 0.3269.
 Standard deviation associated with $\phi_{m,av}$, 0.1523.

^a3.232 movie analyzer units equal 0.75 inch; left end reading, 3.098; right end reading, 6.330 (average right limit, 5.955; reduced area of strip evaluated because of obscuration of film).

TABLE III. - COMPARISON OF THEORETICAL AND EMPIRICAL VARIATION

Run	Average area fraction of merging bubbles, $\phi_{m,av}$	$1 - \phi_{m,av}$	Average area fraction of influence of bubbles, $\phi_{s,av}$	Theoretical variation, $\sigma, \sqrt{\phi_{m,av}(1 - \phi_{m,av})\phi_{s,av}}$	Standard deviation associated with $\phi_{m,av}$, S
62-12-4-1	0.0451	0.955	0.121	0.0722	0.0929
62-12-4-2	.0182	.982	.102	.0426	.0451
62-12-4-3	.0240	.976	.109	.0505	.0649
62-12-4-5	.0402	.960	.138	.073	.0936
62-12-4-6	.0171	.983	.128	.0463	.0533
63-1-14-6	.0291	.971	.143	.0635	.0702
63-2-6-1	.115	.885	.186	.138	.135
63-2-6-2	.255	.745	.185	.188	.225
63-2-6-3	.3695	.630	.208	.220	.214
63-2-6-4	.535	.465	.189	.217	.216
63-7-2-2	.470	.530	.182	.213	.183
63-7-8-1	.110	.890	.109	.103	.117
63-7-8-4	.358	.642	.121	.167	.167
63-7-8-5	.327	.673	.136	.173	.152

11/1/58

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